

**ALGAECULTURE: AN ALTERNATIVE TO SOLVING ENERGY  
SUSTAINABILITY CRISES IN DEVELOPING COUNTRIES**

**ABSTRACT**

There is an impending need to reduce the dependency on fossil fuels in these areas of the world considering the ever depleting conventional oil resources and climate change, induced by greenhouse gas emissions. Algae are currently being prompted as an ideal next generation bioenergy feedstock due to the fact that they do not compete with food or feed crops. They also produce much higher areal oil yields than the current agricultural crops. They can be produced on barren lands and have broad bioenergy potentials as they can be used to produce liquid transportation and heating fuels such as biodiesel and ethanol, or anaerobically digested to produce biogas. Algae are fast growing organisms capable of fixing high amount of carbon dioxide through photosynthesis to produce biomass. Diverse technologies are currently being pursued to produce algae for bioenergy applications.

**KEYWORDS: Algae, Biofuel, Greenhouse, Bioenergy, Feedstock**

**INTRODUCTION**

Escalating fuel prices, the emerging concern about global warming that is associated with burning fossil fuels, quest for economic growth, fighting poverty and the growing demand for petroleum products have spurred new interest in the search for alternative sources of natural oil for fuel (Abubakar *et al.*, 2012). Microalgae are photosynthetic microorganisms that convert sunlight, water and carbon dioxide to algal biomass. Many microalgae are excitingly rich in oil (Chisti, 2007) which can be converted to biodiesel using existing technology. Microalgae are fast growing unicellular or simple multicellular microorganism which have the ability to fix carbondioxide(CO<sub>2</sub>) while capturing solar energy at an efficiency 10 to 50 times greater than that of terrestrial plants and higher biomass production compared to energy crops (Wang *et al.*, 2008). Microalgae are known for their rapid growth and high energy content. The main environmental factors influencing micro algal growth and chemical composition are light,

30 nutrients, temperature and pH (Rousch *et al.*, 2003). Microalgae have several advantages,  
31 including higher photosynthetic efficiency as well as higher growth rates and higher biomass  
32 production compared to other energy crops. Several micro algae strains have been reported to  
33 have the ability to accumulate large quantities of lipids. It has also been observed that nitrogen  
34 limitation leads to an increase of lipid content in some chlorella strains (Reiten *et al.*,  
35 1994). Previous studies have confirmed that lipid content in some micro algae strains could be  
36 increased by various cultivation conditions (Illman *et al.*, 2000), under stress conditions a lipid  
37 production of 30%-60% of dry cell weight has been reported, one can only imagine the yields  
38 under favourable conditions. Since fatty acid methyl esters originating from vegetable oils and  
39 animal fats are known as biodiesel, from the energetic point of view, lipids are the most desirable  
40 components of microalgae cells (Sostaric *et al.*, 2009). In addition the organic matter produced by  
41 photosynthetic microalgae can be transformed into a wide range of valuable products, such as  
42 biodiesel, food additives and health-care products (Pulz and Gross, 2004). Algal-oil processes  
43 into biodiesel as easily as oil derived from land-based crops. Algae have much faster growth rates  
44 than terrestrial crops. The per unit area yield of oil from algae is estimated to be from between  
45 5,000 to 20,000 gallons (18,927 to 75,708 litres) per acre, per year; this is 7 to 31 times greater  
46 than the next best crop, palm oil (635 gallons or 2,404 litres). Many companies are pursuing the  
47 development of algae bioreactors for various purposes, including biodiesel production and CO<sub>2</sub>  
48 capturing (Veridium Patents Yellowstone, 2007). This paper highlights the potential of  
49 microalgae for sustainably providing biodiesel for displacement of petroleum-derived transport  
50 fuels, such as gasoline, jet fuel and diesel.

51

## 52 **Algae Cultivation**

### 53 **Raceway Ponds**

54 A raceway pond is made of a closed loop recirculation channel that is typically about 0.3m deep.  
55 Mixing and circulation are produced by a paddlewheel. Flow is guided around bends by baffles  
56 placed in the flow channel. Raceway channels are built in concrete or compacted earth, and may  
57 be lined with white plastic. Broth is harvested behind the paddlewheel, on completion of the  
58 circulation loop. The paddlewheel operates all the time to prevent sedimentation. Raceway ponds  
59 for mass culture of microalgae have been used since the 1950s. Extensive experience exists on  
60 operation and engineering of raceways. Evaporative water loss can be significant. Because of

61 significant losses to atmosphere, raceways use carbon dioxide much less efficiently than photo-  
62 bioreactors. Productivity is affected by contamination with unwanted algae and microorganisms  
63 that feed on algae. The biomass concentration remains low because raceways are poorly mixed  
64 and cannot sustain an optically dark zone. Raceways are perceived to be less expensive than photo-  
65 bioreactors, because they cost less to build and operate. Although raceways are low-cost, they  
66 have a low biomass productivity compared with photo-bioreactors.

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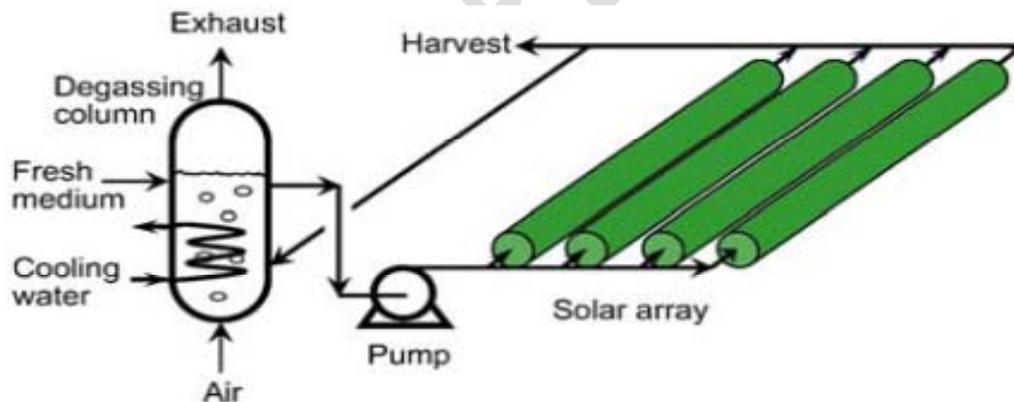
## 68 **Photo-bioreactors**

69 Unlike open raceways, photo-bioreactors permit essentially single-species culture of microalgae  
70 for prolonged durations. Photo-bioreactors have been successfully used for producing large  
71 quantities of microalgal biomass (Carvalho *et al.*, 2006).

72 A tubular photo-bioreactor consists of an array of straight transparent tubes that are usually made  
73 of plastic or glass. This tubular array, or the solar collector, is where the sunlight is captured (Fig.  
74 1). The solar collector tubes are generally 0.1 m or less in diameter. Tube diameter is limited  
75 because light does not penetrate too deeply in the dense culture broth that is necessary  
76 for ensuring a high biomass productivity of the photo-bioreactor.

77 Microalgal broth is circulated from a reservoir to the solar collector and back to the reservoir.

78



79

80 Figure 1: A tubular photobioreactor with parallel run horizontal tubes

81 The solar collector is oriented to maximize sunlight capture (Molina *et al.*, 1999; Sánchez *et al.*,  
82 1999). In a typical arrangement, the solar tubes are placed parallel to each other and flat above the  
83 ground (Fig. 1). Horizontal, parallel straight tubes are sometimes arranged like a fence, in  
84 attempts to increase the number of tubes that can be accommodated in a given area. The ground  
85 beneath the solar collector is often painted white, or covered with white sheets of plastic (Tredici,

1999), to increase reflectance, or albedo. A high albedo increases the total light received by the tubes. Biomass sedimentation in tubes is prevented by maintaining highly turbulent flow. Flow is produced using either a mechanical pump (Fig. 1), or a gentler airlift pump. Mechanical pumps can damage the biomass (Mazzuca *et al.*, 2006), but are easy to design, install and operate.

**Table 1: Comparison of photo-bioreactor and raceway production methods**

VARIABLE	PHOTO-BIOREACTOR FACILITY	RACEWAY PONDS
Annual biomass production (kg)	100,000	100,000
Volumetric productivity (kg/m <sup>3</sup> /d)	1.535	0.117
Areal productivity (kg/m <sup>2</sup> /d)	0.048 <sup>a</sup> 0.072 <sup>c</sup>	0.035 <sup>b</sup>
Biomass concentration in broth (kg/m <sup>3</sup> )	4.00	0.14
Area needed (m <sup>2</sup> )	5681	7828
Oil yield (m <sup>3</sup> /ha)	136.9 <sup>d</sup> 58.7 <sup>e</sup>	99.4 <sup>d</sup> 42.6 <sup>e</sup>
Annual CO <sub>2</sub> consumption (kg)	183,333	183,333
Number of units	6	8

<sup>a</sup> Based on facility area.

<sup>b</sup> Based on actual pond area.

<sup>c</sup> Based on projected area of photo-bioreactor tubes.

<sup>d</sup> Based on 70% by wt oil in biomass.

<sup>e</sup> Based on 30% by wt oil in biomass.

(Christi, 2007)

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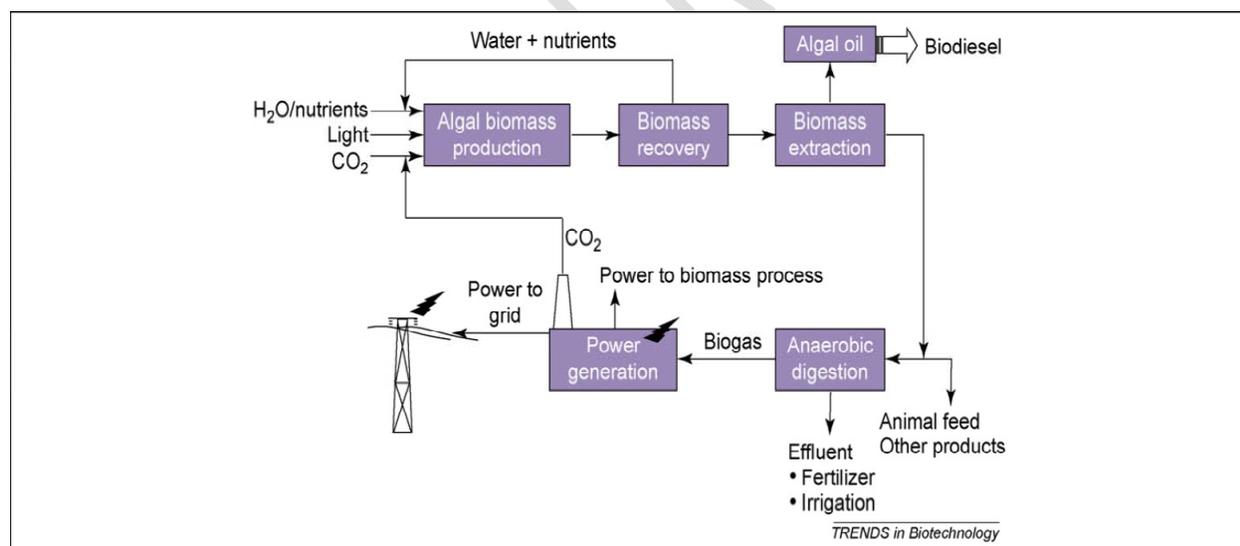
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## 102 Algae Oils

103 Oil content of some microalgae exceeds 80% of the dry weight of algae biomass. Agricultural oil  
104 crops, such as soybean and oil palm, are widely being used to produce biodiesel; however, they  
105 produce oils in amounts that are miniscule (e.g. less than 5% of total biomass basis) compared  
106 with microalgae (Chisti, 2007). As a consequence, oil crops can provide only small quantities of  
107 biodiesel for blending with petroleum diesel at a level of a few percent, but they are incapable of  
108 providing the large quantities of biodiesel that are necessary to eventually displace all petroleum-  
109 sourced transport fuels (Chisti, 2007).

110 A conceptual process for producing microalgal oils for making biodiesel is shown in Plate 1. The  
111 process consists of a microalgal biomass production step that requires light, carbon dioxide,  
112 water and inorganic nutrients. The latter are mainly nitrates, phosphates, iron and some trace  
113 elements. Sea water supplemented with commercial nitrate and phosphate fertilizers, and a few  
114 other micronutrients, is commonly used for growing marine microalgae (Molina *et al.*, 1999).

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118 Plate 1: A conceptual process for producing microalgal oil for biodiesel

119 Approximately half of the dry weight of the microalgal biomass is carbon (Sanchez. *et al.*, 2003),  
120 which is typically derived from carbon dioxide. Therefore, producing 100 tons of algal biomass  
121 fixes roughly 183 tons of carbon dioxide. This carbon dioxide must be fed continually during  
122 daylight hours. Microalgal biomass production can potentially make use of some of the carbon  
123 dioxide that is released in power plants by burning fossil fuels (Sawayama *et al.*, 1995). The

124 algal broth produced in the biomass production stage needs to be further processed to recover the  
125 biomass (Molina *et al.* 2003). The water and residual nutrients recovered at this stage can be  
126 recycled to the biomass-cultivation. The concentrated biomass paste is extracted with a water-  
127 immiscible solvent to recover algal oil, which can then be converted to biodiesel. The biomass  
128 residue that remains after extraction of oil could be used partly as high-protein animal feed and,  
129 possibly, as a source of small amounts of other high-value microalgal products (Gavrilescu and  
130 Chisti, 2005). In both scenarios, the revenue from selling the biomass residues could defray the  
131 cost of producing biodiesel. However, the majority of algal biomass residue from oil extraction is  
132 expected to undergo anaerobic digestion to produce biogas. The carbon dioxide generated from  
133 combustion of biogas can be recycled directly for the production of the microalgae biomass.  
134 Energy content of biogas produced through anaerobic digestion typically ranges from  
135 16200kJ/m<sup>3</sup> to 30600kJ/m<sup>3</sup>(Wulf, 2005) depending on the nature of the source biomass.  
136 Typically, the yield of biogas varies from 0.15 to 0.65kg of dry biomass (Wulf, 2005). Assuming  
137 average values of biogas energy content and yield, biogas production from microalgal solids,  
138 after their 30% oil content has been removed, could provide at least 9360MJ of energy per metric  
139 ton. This is a substantial amount of energy and it should run the microalgal biomass production  
140 process. The total content of lipids in microalgae vary from about 1-85% of the dry weight  
141 (Rodolfi *et al.*, 2009) with values higher than 40% typically achieved under nutrient limitation.

142

### 143 **Algae for Biofuels**

144 Algae for biofuels have been studied for many years for production of hydrogen, methane,  
145 vegetable oils (triglycerides, for biodiesel), hydrocarbons and ethanol. Methane was the focus of  
146 most of the early work in microalgae biofuels production, when microalgae were considered  
147 mainly for their applications in wastewater treatment. More simply would be the production of  
148 starch by microalgae and its subsequent fermentation by yeasts, as practiced with cane sugar and  
149 corn starch in fuel ethanol production. Such an approach, however, would compete with very  
150 low-cost sugar and starch produced by higher plants. It is, however, not all that different in  
151 concept from the production of vegetable oils, triglycerides specifically, which is the focus of  
152 almost all the current interest in algae biofuels.

153

## 154 **Bioenergy Conversion of Algae**

155 Biomass from micro- and macroalgae can be converted into solid, liquid or gaseous energy  
156 carriers but there are some major differences in the chemical and physical chemical composition  
157 of algae as well as their physical composition which make them more or less suitable for a given  
158 conversion technology.

159 In general the most important issues to remember when evaluating bioenergy conversion  
160 technologies for algae are their high content of inorganics (more than 30% can be found), a low  
161 level of fermentable sugars, high protein and sulphur content and a potentially very high content  
162 of oils. The glycerine has many uses, such as in the manufacture of food, in the production of  
163 pharmaceuticals as well as a feedstock for biogas.

164

## 165 **Algae Biodiesel**

166 The term bio-diesel covers diesel type oil made from vegetable oils. In plants oils are found as  
167 triglycerides, where three fatty acids of different chain lengths are coupled to a glycerol molecule  
168 by ester bonds. By splitting the triglycerides into their components via a transesterification  
169 reaction the single fatty acids can be separated for used as fuel in diesel engines. In principle the  
170 plant oils can be used directly as diesel fuels, but triglycerides have a high melting point and can  
171 be solid at low temperatures.

172

## 173 **Algae ethanol**

174 The production of ethanol by fermentation of sugars is technically well developed. On  
175 commercial scale the sugar glucose is fermented by ordinary yeast to produce ethanol. Glucose is  
176 a so called C6 sugar with 6 carbon atoms and can be found in a number of different plant sugars  
177 of which cellulose, starch and sucrose are the most common. New microorganisms capable of  
178 fermenting C5 sugars are under development, but have not yet reached a commercial scale and  
179 applicability.

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## 181 **Combustion**

182 Efficient combustion of biomass requires a low content of inorganic components as well as of  
183 nitrogen and sulphur compounds. The chemical composition of algae biomass shows that it is not  
184 a suitable feedstock for combustion. Raw algae biomass is thus not suitable for heat and

185 electricity production by combustion. No reports on combustion of algae biomass have been  
186 found.

187

## 188 **Biogas**

189 Biogas is produced by methanogenic bacterial breakdown of organic matter under anaerobic  
190 conditions. It is also known as anaerobic digestion or mesophilic fermentation, and consists of at  
191 least three bacterial processes yielding the main final products methane (CH<sub>4</sub>) and CO<sub>2</sub>. A wide  
192 range of organic matter can be converted in a biogas reactor, with lignin and cellulose being the  
193 main exceptions. The processing of biomass in a biogas reactor typically takes weeks, but the  
194 process as such is robust. The composition of biogas varies depending upon the feedstock.  
195 Biogas will contain CH<sub>4</sub>, CO<sub>2</sub>, H<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub>, H<sub>2</sub>S and water vapour. Typically the methane content  
196 of biogas is 55-75% CH<sub>4</sub>, 20-40% CO<sub>2</sub> and smaller amounts of the other gases. Purification of  
197 the gas is therefore needed and several large-scale methods are available. Following the  
198 conversion to biogas there will be residual liquid and fibre fractions. The liquid fraction typically  
199 has a high content of salts and nitrogen, whereas the fibre fraction contains the biomass that  
200 could not be digested by the bacteria.

201 Biogas production from of algae by methanogenic bacteria is probably the best suited technology  
202 for converting both macro- and microalgae biomass into a practical energy carrier.

203

## 204 **Algae Harvesting and Strains**

205 The basic concept of algal oil production is to use relatively small (in total area) photo-  
206 bioreactors to produce a modest amount of “inoculum” culture (about 1-2 % of the total biomass  
207 produced) to seed much larger, totaling several hundred hectares, open ponds. The biomass  
208 would need to be concentrated by an initial factor of at least about thirty-fold, requiring very  
209 low-cost harvesting processes, such as “bioflocculation”, a spontaneous flocculation-  
210 sedimentation of the algal cells, using no, or at most very little, flocculation chemicals. Such  
211 low-cost harvesting processes must be developed and demonstrated for each algal species and  
212 even strain. At present there are no low-cost harvesting technologies available. The algal strains  
213 to be cultivated would be selected based on many criteria, of which oil content, productivity, and  
214 harvestability would be primary, but also resistance to contamination, tolerance of high oxygen  
215 levels and temperature extremes, and adaptation to the local water chemistry and other local

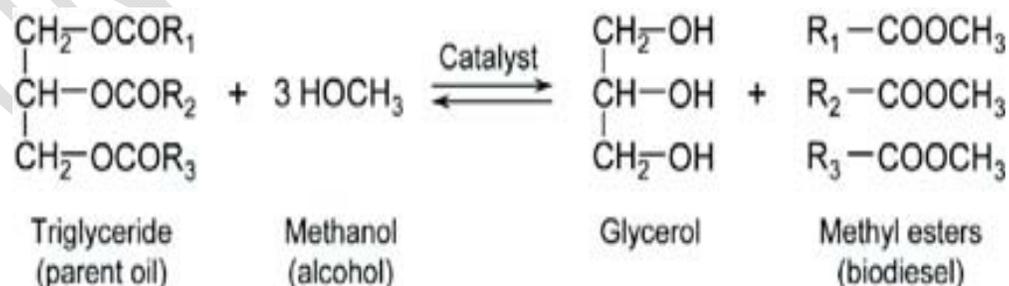
216 conditions experienced by the algal cells in the growth ponds. Figure 2 shows microalgal  
 217 biomass being recovered from the culture broth by filtration  
 218 After harvesting, further concentration and oil extraction is required, for which various processes  
 219 are proposed, including cell breakage and solvent extraction, possibly using a three phase  
 220 centrifugation.  
 221



222  
 223 Figure 2: Microalgal biomass recovered from the culture broth by filtration

### 224 Biodiesel Production

225 Parent oil used in making biodiesel consists of triglycerides in which three fatty acid molecules  
 226 are esterified with a molecule of glycerol. In making biodiesel, triglycerides are reacted  
 227 with methanol in a reaction known as trans-esterification or alcoholysis. Trans-esterification  
 228 produces methyl esters of fatty acids that are biodiesel, and glycerol (Figure 3).  
 229 The reaction occurs stepwise: triglycerides are first converted to diglycerides, then to  
 230 monoglycerides and finally to glycerol.



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Figure 3: Trans-esterification of oil to biodiesel (R1-3 are hydrocarbon groups).

234 Trans-esterification requires 3 mols of alcohol for each mole of triglyceride to produce 1 mol of  
235 glycerol and 3 mols of methyl esters (Fig. 3). Industrial processes use 6mol of methanol for each  
236 mole of triglyceride (Fukuda *et al.*, 2001). Yield of methyl esters exceeds 98% on a weight basis  
237 (Fukuda *et al.*, 2001).

238 Trans-esterification is catalyzed by acids, alkalis (Meher *et al.*, 2006) and lipase enzymes  
239 (Sharma *et al.*, 2001). Alkali-catalyzed trans-esterification is about 4000 times faster than the  
240 acid catalyzed reaction (Fukuda *et al.*, 2001). Alkali-catalyzed trans-esterification is carried out  
241 at approximately 60°C under atmospheric pressure; as methanol boils off at 65°C at atmospheric  
242 pressure. A higher temperature can be used in combination with higher pressure, but this is  
243 expensive. Methanol and oil do not mix; hence the reaction mixture contains two liquid phases.

244 The main advantages with producing micro algae for energy production are:

- 245 • Does not compete with agriculture
- 246 • High per acre yield
- 247 • Contains no Sulphur therefore no SO<sub>2</sub> emissions
- 248 • Nontoxic and highly biodegradable
- 249 • Does not require soil for growth
- 250 • Uses as little as 8cm of water per year
- 251 • Adaptable anywhere even at great distances from water.
- 252 • Industrial emissions of CO<sub>2</sub> from power plants, refineries, and other stationary emitters  
253 can be productively consumed by micro algae in engineered plants and used to  
254 manufacture valuable products, thus making the whole process carbon neutral.

255  
256 Hundreds of species of micro algae are being experimented with, such as *Arthrospira*  
257 *platensis* (spirulina) which is easy to culture and easy to harvest but does not contain a high oil  
258 content and *Haematococcus pluvialis* (red algae), which is very high in oil yield.  
259 With the correct species in place and the right conditions the species can produce oil at near-  
260 theoretical limits

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265 **Table 2:** Oil content of some microalgae

MICROALGA	OIL CONTENT (% DRY WT)
<i>Botryococcus braunii</i>	25–75
<i>Chlorella sp.</i>	28–32
<i>Cylindrotheca sp.</i>	16–37
<i>Isochrysis sp.</i>	25–33
<i>Nannochloropsis sp.</i>	31–68
<i>Schizochytrium sp.</i>	50–77

266 Modified from Chisti (2007).

267

## 268 **Economics of Biodiesel Production**

269 Recovery of oil from microalgal biomass and conversion of oil to biodiesel are not affected by  
 270 whether the biomass is produced in raceways or photo-bioreactors. Hence, the cost of producing  
 271 the biomass is the only relevant factor for a comparative assessment of photo-bioreactors and  
 272 raceways for producing Microalgal biodiesel. For the facilities detailed in Table 1, the estimated  
 273 cost of producing a kilogram of microalgal biomass is \$2.95 (N442.5) and \$3.80 (N570) for  
 274 photo-bioreactors and raceways, respectively (Chisti, 2007). If the annual biomass production  
 275 capacity is increased to 10,000 tonnes, the cost of production per kilogram reduces to roughly  
 276 \$0.47 (N70.5) and \$0.60 (N90) for photo-bioreactors and raceways, respectively, because of  
 277 economy of scale. Assuming that the biomass contains 30% oil by weight, the cost of biomass  
 278 for providing a liter of oil would be about \$1.40 (N210) and \$1.81 (N271.5) for photo-  
 279 bioreactors and raceways, respectively (Chisti, 2007). Oil recovered from the lower-cost biomass  
 280 produced in photo-bioreactors is estimated to cost \$2.80/L (N420/L). Biodiesel from palm oil  
 281 costs roughly \$0.66/L (N99/L) or 35% more than petro-diesel. This suggests that the process of  
 282 converting palm oil to biodiesel adds about \$0.14/L (N21/L) to the price of oil. For palm oil  
 283 sourced biodiesel to be competitive with petro-diesel, the price of palm oil should not exceed  
 284 \$0.48/L (N72/L).

285 Microalgal oils can potentially completely replace petroleum as a source of hydrocarbon  
 286 feedstock for the petrochemical industry. For this to happen, Microalgal oil will need to be  
 287 sourced at a price that is roughly related to the price of crude oil. For example, if the prevailing  
 288 price of crude oil is \$60/barrel (N9000/barrel), then microalgal oil should not cost more than  
 289 about \$0.41/L (N61.5/L), if it is to substitute for crude oil. If the price of crude oil rises to

290 \$80/barrel (N12000/L) as sometimes predicted, then microalgal oil costing \$0.55/L (N82.5/L) is  
291 likely to economically substitute for crude petroleum.

292

## 293 **CONCLUSION**

294 Algal biodiesel is technically feasible. Producing low-cost microalgal biodiesel requires primarily  
295 improvements to algal biology through genetic and metabolic engineering.

296 Biodiesel has great potential; however, the high cost and limited supply of organic oils prevent it  
297 from becoming a serious competitor for petroleum fuels. As petroleum fuel costs rise and  
298 supplies dwindle, alternative fuels will become more attractive to both investors and consumers.

299 For biodiesel to become the alternative fuel of choice, it requires an enormous quantity of cheap  
300 biomass. Using new and innovative techniques for cultivation, algae may allow biodiesel  
301 production to achieve the price and scale of production needed to compete with, or even  
302 replace, petroleum. Algal biomass needed for production of large quantities of biodiesel could be  
303 grown in photo-bioreactors, but a rigorous assessment of the economics of production is necessary  
304 to establish competitiveness with petroleum-derived fuels. Achieving the capacity to  
305 inexpensively produce biodiesel from microalgae is of strategic significance to an  
306 environmentally sustainable society.

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