Original Research Article

Validating Visual Modflow Numerical Model To Predict Future

Impact Of Brine Disposal On Groundwater

ABSTRACT

The aim of this research is to simulate the groundwater extraction and brine disposal fate. The Visual MODFLOW numerical model was used to predict the salt concentration emigration over time in an aquifer. The main objective of this study is to check the validity of using a numerical model in predicting the impact of brine disposal on the groundwater salinity. A numerical modelling study was carried to simulate the groundwater extraction and brine disposal using Visual MODFLOW and it was calibrated using a laboratory experiment results. The model results revealed that there was a great agreement between the results obtained from the model and the laboratory experiment where the correlation coefficient obtained from the model for the COB3 was 0.991, while for HOB1 was 0.901.

Keywords: Desalination; Injection well; discharge well; salt concentration; aquifer

INTRODUCTION

Water desalination is one of the non-conventional water resources where fresh water is produced from treatment of salt water. However, the negative impact of desalination process is the brine disposal which is a real environmental problem that should be considered and studied before constructing a desalination plant. The brine resulted from the desalination process is usually injected into aquifer or discharged into the sea. The practice of disposing the rejected brine into the sea is common for plants located in coastal areas [3]. The problem of disposing the rejected brine into the sea may increase seawater salinity leading to injuring plants and animals in the marine sanctuary [7,9,11]. In the case of disposing the rejected brine into the ground, it is necessary to design a disposal system in a way that respects the environment.

Numerical groundwater models have been used in developed countries since 1970's. Afterwards, there has been an increase in the usage of groundwater models, especially MODFLOW to address a wide range of water-related problems. [8] assessed the behaviour of production and injection well of desalination plants through an experimental setup and computational simulation. Their results showed that the injection well will affect the salinity of the production well on the long run. [1] used MODFLOW to simulate groundwater extraction for managing groundwater level in Jordan Valley. [5] developed a mathematical groundwater model for the Mahesh River basin in the Akola and Buldhana districts using a MODFLOW model to predict the groundwater levels variation under different hypothesis conditions to manage the groundwater. [10] used MODFLOW to develop a model for the study area to determine the interaction between the surface water and groundwater. [2] developed a mathematical model for the Upper Awash river basin using the MODFLOW then calibrated it in order to manage the sustainable groundwater resource of the country.

Calibration/validation has become a practice to ensure a model represents the observed groundwater conditions of a studied area. Model calibration is the process where values of model inputs are adjusted so that the model matches the observed data [6]. In this research, the laboratory experiment of [8] is used to calibrate the Visual MODFLOW (VMOD) model. The main objective of this study is to check the validity of using a numerical model in predicting the impact of brine disposal on the groundwater salinity.

VISUAL MODFLOW MODEL

Visual MODFLOW is a software developed by Waterloo Hydro geologic. The software is used to simulate three-dimensional groundwater movement and solute transport. Visual MODFLOW provides many numeric engines that perform the numeric calculations required to solve the finite difference scheme of groundwater flow and mass transport. SEAWAT is the numerical engine implemented in this study as it simulates three-dimensional, variable-density, unsteady groundwater flow in porous media. The density-dependent groundwater flow model is governed by the equation developed by [2] as shown in

50 Eq. (1)

$$51 \qquad \frac{\partial}{\partial x} \left(\rho K_{fx} \left[\frac{\partial h_f}{\partial x} \right] \right) + \frac{\partial}{\partial y} \left(\rho K_{fy} \left[\frac{\partial h_f}{\partial y} \right] \right) + \frac{\partial}{\partial z} \left(\rho K_{fz} \left[\frac{\partial h_f}{\partial z} + \left(\frac{\rho - \rho_f}{\rho_f} \right) \right] \right) = \rho s_f \frac{\partial h_f}{\partial t} + \theta \frac{\partial \rho}{\partial c} \frac{\partial c}{\partial t} - \underline{\rho} q_s \qquad (1)$$

Where ρ is the fluid density, K_{fx} , K_{fy} and K_{fz} are freshwater hydraulic conductivity in the x, y and z direction, h_f is the equivalent fresh water head, ρ_f is the density of freshwater, S_f is the fresh water specific storage, θ is the porosity, C is the concentration of solute mass per unit volume of fluid, q_s is the

volumetric flow rate of sources or sinks per unit volume of aquifer and t is time. The governing equation

for solute-transport is given by Eq. (2):

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$$\frac{\partial(\theta C)}{\partial t} = \nabla(\theta D. \nabla C) - \nabla(qC) \pm q_s C_s$$
 (2)

- 58 Where:
- D is the hydrodynamic dispersion coefficient tensor, q is specific discharge and
- 60 C_s is the solute concentration of water entering from sources or sinks.

61 **NUMERICAL MODEL**

- Brine disposal by injection well in a coarse sand soil has been studied by [8] at Hydraulic Laboratory of 62 63 Cairo University, Giza, Egypt using a rectangular seepage tank with dimension of 1.42 m long, 0.1 m 64 wide and 0.6 m high. An injection well of 10 cm width was inserted on the left side of the seepage tank 65 with a screen of 10 cm width that located at 0.15 m from the base of the tank. While, a constant head 66 boundary of 24.5 cm was maintained on the right side of the tank. A constant head reservoir containing 67 brine water of 39,400 ppm concentration was used to feed the injection well at a rate of 0.144 m3/day. 68 Several observation points were constructed within the seepage tank to get the observed values of head 69 and salt concentration as shown in Table 1. The head observed value and the salt concentration 70 observed value at the specified location and time has been recorded by a sounder and a digital 71 conductivity meter respectively. A numerical model was built to simulate the laboratory experiment 72 using Visual MODFLOW as shown in the following section.
- 73 Models domain
- 74 As shown in Fig.1 the model domain consists of one row, 29 columns and five layers. Each cell, with the
- 75 exception of the cells in column 1 and cells in layer 1, is 0.05 * 0.05 m in size. Cells in column 1 are
- 76 0.02m * 0.05m and cells in layer 1 are 0.05m * 0.2m.

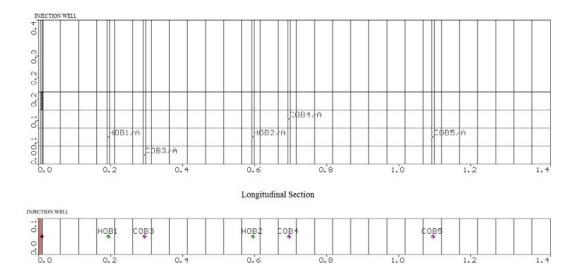


Fig.1. Model grids layout

Plan view

Initial and boundary conditions

Initial water concentrations of model domain are set to be 800 mg/l and initial fresh water heads are all set to be 0.245 m. Brine is applied in column one and layer two through a well with injection rate 0.144 m³/day and of concentration equal to 39400 mg/l. A constant fresh water head boundary of 0.245 m and a constant concentration equal to 800 mg/l are specified at column 29 and layer one.

Model parameters

The parameters used in this model are hydraulic conductivity which is generally uniform and isotropic, specific yield, porosity and coefficient of effective molecular diffusion. The assigned values for these parameters were set to be 83 m/day, 0.27, 0.3 and 8.53*10⁻⁸ m²/min respectively.

Observation Points

Several observation points were constructed within the model domain as shown in Fig.1 and Table 1.

Table 1. Observation points locations

•	Observation Point No.	Observation point type	X (cm)	Y (cm)	Z (cm)
	HOB1	Head	19.5	5	7.5
	HOB2	Head	59.5	5	7.5
	COB3	Salt conc.	29.5	5	2.5

	COD-1	Sait conc.	03.3	3	12.3	
	COB5	Salt conc.	109.5	5	7.5	
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92	MATHEMATICAL MODEL CA	<mark>LIBRATION</mark>				
93	In order to calibrate the nu	merical model, the	initial and	<mark>boundar</mark>	y conditions	s of the laboratory
94	experiment were assigned. Inj	ection well (injection	n rate 0.144	m3/day	<mark>/ and of cor</mark>	centration equal to
95	39400 mg/l) and different obs	ervation points were	represente	d in the	model as sp	pecified by [8]. The
96	records obtained from the l	head and concentra	tion observ	<mark>/ation p</mark>	oints are r	equired during the
97	97 calibration process of the Visual MODFLOW model.					
98	Time steps were set to be 24 st	teps to represent bot	h head and	concenti	ration values	for six hours model
99	run.					
100	Results of calibration					
101	The outputs of the model are i	llustrated in Fig. <mark>2</mark> and	d Fig. <mark>3</mark> . A c	omparis	on between	the results obtained
102	from the VMOD and the labor	ratory experiment of	[<mark>8</mark>] for the	concent	ration obser	vation points COB3,
103	COB4 and COB5 is shown in Fig	. <mark>2</mark> .				
104	The correlation coefficient obt	ained from the mode	el for these	observat	tion points v	vere equal to 0.991,
105	0.995 and 0.981 respectively.	While, Fig. <mark>3</mark> shows a	comparisor	n betwee	n the result	s obtained from the
106	VMOD and the laboratory ex	periment of [<mark>8</mark>] for	the head o	bservati	on points H	OB1 and HOB2.The
107	correlation coefficient obtaine	d from the model for	r HOB1 equ	al to 0.9	01and for H	OB2 equal to 0.835.

Salt conc.

69.5 5

12.5

COB4

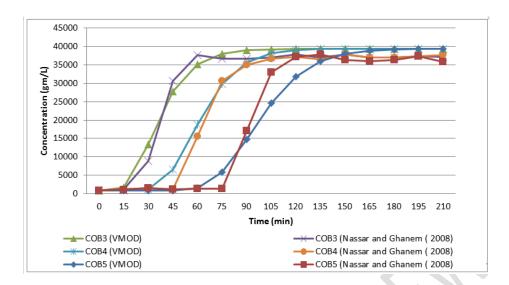


Fig. 2. Comparison between results of Visual MODFLOW and laboratory experiment of [8] for COB3,

110 COB4 and COB5

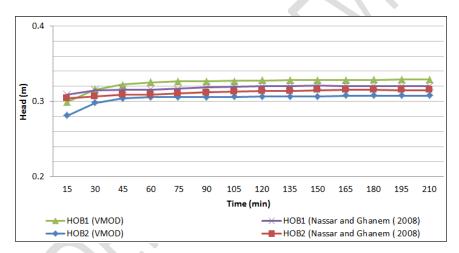


Fig. 3. Comparison between results of Visual MODFLOW and laboratory experiment of [8] for HOB1 and HOB2

CONCLUSIONS

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From this study we can conclude that:

 There was a great agreement between the results of the Visual MODFLOW and that of the laboratory experiment, where the correlation coefficient obtained from the model for the COB3, COB4 and COB5 were 0.991, 0.995 and 0.981 respectively. While for HOB1 and HOB2 were 0.901 and 0.835 respectively. 120 2. The Visual MODFLOW can assist engineers and researchers in simulating and predicting the 121 future impact of brine disposal on the groundwater salinity. 122 Competing interests: no competing interests exist 123 **REFERENCES** 124 1. Alfaro P, Liesch T, Goldscheider N. Modelling groundwater over-extraction in the southern 125 Jordan Valley with scarce data. Hydrogeology Journal, 2017;25(5):1319-1340. 126 https://doi.org/10.1007/s10040-017-1535-y 127 2. Berehanu B, Ayenew T, Azagegn T. Challenges of Groundwater Flow Model Calibration Using 128 MODFLOW in Ethiopia: With Particular Emphasis to the Upper Awash River Basin. Journal of 129 Geoscience and Environment Protection. 2017;05(03):50-66. 130 https://doi.org/10.4236/gep.2017.53005 131 3. El-Naas M H, Al-Marzougi A H, Chaalal O. A combined approach for the management of 132 CO2. Desalination. desalination reject brine and capture of 2010:251:70-74. 133 https://doi.org/10.1016/j.desal.2009.09.141 134 4. Guo W, Langevin C D. User's guide to SEAWAT: a computer program for simulation of three-135 dimensional variable-density ground-water flow. USGS Techniques of Water Resources 136 Investigations chap A7. 2002. 137 5. Khadri S F R, Pande C. Ground water flow modeling for calibrating steady state using 138 MODFLOW software: a case study of Mahesh River basin, India. Modeling Earth Systems and 139 Environment, 2016; 2:39. https://doi.org/10.1007/s40808-015-0049-7 140 Maliva, Robert G., Missimer, Thomas M. Arid Lands Water Evaluation and Management. 141 Springer; 2012 142 7. Mansour S, Arafat H A, Hasan S W. Brine Management in Desalination Plants. In Desalination 143 Sustainability. Elsevier. 2017;207–236. https://doi.org/10.1016/B978-0-12-809791-5.00005-5 144 8. Nassar M K K, El-Damak R M, Ghanem A H M. Impact of desalination plants brine injection wells 145 on coastal aquifers. In Environmental Geology. 2008;54:445-454. 146 https://doi.org/10.1007/s00254-007-0849-9

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