

Studies of the Nutritional, Environmental Effects and Repressive nature of Simple Sugars on the Production of endo- β -mannanase by *Aspergillus flavus* PT7 on Solid State Fermentation.

ABSTRACT

Aims: The importance of nutritional and environmental factors in the production of microbial enzymes cannot be overemphasized. Hence, endo- β -mannanase production was systematically studied in a step-wise approach of building up on the experimentally observed conditions favouring the production of this enzyme in *Aspergillus flavus* PT7.

Place and Duration of Study: Department of Microbiology, University of Ibadan, Nigeria, between January 2018 and December 2018.

Methodology: Thirty-eight (38) fungal isolates obtained were screened for mannolytic ability using standard method. The highest producer of endo- β -mannanase was subjected to various production conditions by adjusting the nutritional and environmental factors in view of optimizing the production of this enzyme in the isolate *Aspergillus flavus* PT7.

Results: Copra meal was the highest inducer of mannanase production in the isolate at enzyme activity of 85.86 ± 3.93 U/gds. Production increased to 94.54 ± 0.42 when all forms of extraneous nitrogen sources were excluded from the production medium. pH 5.0, temperature 30°C , moisture content at 100% v/w and inoculum size of 8.0% v/w led to the increase in production by 44% (enzyme activity of 153.24 ± 5.69 U/gds) in 5 days of incubation. Allowing the production set up additional two (2) days led to production increase with a recorded enzyme activity of 170.34 ± 4.35 U/gds. Production of endo- β -mannanase in *A. Flavus* PT7 was observed to be inductive as the presence of simple sugars like glucose, galactose, arabinose and xylose led to extended lag period in the production of the enzymes by the isolate.

Conclusion: Production of endo- β -mannanase by *Aspergillus flavus* PT7 was successfully optimized in a step-wise and systematic experimental study of the nutritional and environmental growth conditions of the isolate.

Keywords: *Aspergillus flavus* PT7, Optimization, Fermentation, Agro waste

1. INTRODUCTION

Mannans are the second most abundant hemicellulosic polysaccharides in nature. They are usually encountered in the following families: pure mannan, glucomannan, galactoglucomannan and galactomannan, depending on their biological origin [1]. Mannan exists as non-starchy carbohydrates in cell walls of some plants. They are the major polysaccharides of leguminous seeds, coconut and palm kernel seeds, konjac tubers and guar plants. Mannans are found in plants such as the seed endosperm of certain plant species [2] and have been isolated from ivory nut (*Phytelephas macrocarpa*), date (*Phoenix dactylifera*) and green coffee bean (*Coffea arabica*). They are the major structural units in woods and seeds of these plants [3].

The major enzymes required for the hydrolysis of mannan containing plant biomasses into simple sugars are endo-1, 4- β -mannanases (EC 3.2.1.78) and exo-1, 4- β -mannosidases (EC 3.2.1.25). These two enzymes act on the

27 polymeric backbone of the mannan polysaccharide resulting in the release of manno-oligosaccharides, manno-
28 dissaccharides and mannose. However, additional enzymes including β -glucosidases (EC 3.2.1.21), α -galactosidases
29 (EC 3.2.1.22) and acetyl mannan esterases are needed to cleave off the side chain sugars attached at different points
30 on the backbone of mannan polysaccharides to allow a more effective hydrolysis of the plant polymer [4].

31 Microorganisms producing mannanases are ubiquitous in nature as this enzyme is elaborated by compendia of
32 microorganisms largely isolated from natural environments [4]. A vast variety of bacteria, actinomycetes, yeast and
33 fungi are known to be mannanase producers [5]. Various mannanases have been produced from *Streptomyces sp.* [6],
34 *Bacillus subtilis* [7], *Sclerotium (Athelia) rolfsii* [8], *Aspergillus awamori* [9] and *Trichoderma harzianum* [10].

35 Mannanases have found biotechnological applications in several industrial processes such as food, feed, and
36 pulp and paper industries [11]. However, the application of mannanase is still limited due to low yields and high-
37 production costs [12]. This problem can be mitigated by sourcing for efficient mannanase enzyme producer. Haung
38 and Monk [13] asserted that the best way to source for efficient lignocellulytic microorganisms is to isolates them from
39 lignocellulose biomasses as well. Hence, this work was then designed to source for and produce high levels of
40 mannanase from fungal isolates obtained from degrading mannan-substrates.

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42 **2. MATERIAL AND METHODS**

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44 **2.1 Sample procurement**

45 Copra meal, palm kernel cake, potato peels and soybean meal were obtained from Bodija Market within Ibadan
46 metropolis and transported to the Laboratory in clean polythene bags. Locust Bean Gum was purchased from Sigma
47 Chemicals (St. Louis, Mo, USA). All other chemicals were of analytical grade.

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49 **2.2 Source of Microorganisms**

50 Mannan degrading fungal species used for this work where isolated from degrading Palm Kernel Cake (PKC) and
51 Potato Peels (PT).

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53 **2.3 Isolation of Microbial Isolates**

54 The isolation of mannan degrading fungi was carried out on selective medium ML1 [14] using decaying PKC and PT as
55 supplemented carbon sources at different instances. One (1) gram of each of the samples was suspended in 9 mL of
56 sterile distilled water and agitated vigorously for about 15 minutes. One milliliter of the resulting liquid was transferred
57 to ML1 medium using pour plating technique (Kheng and Ibrahim, 2005). The selective medium ML1 was prepared
58 with the following composition (g/L) PKC or PT, 6.0; yeast extract, 0.5; casein peptone, 1.0; KH_2PO_4 , 1.0; $(\text{NH}_4)_2\text{HPO}_4$,
59 1.0; $\text{MgSO}_4 \cdot \text{H}_2\text{O}$, 0.7; agar, 15.0. All plates were incubated inverted at 30°C for 3 to 5 days. Distinctive fungal colonies
60 were sub-cultured on Malt Extract agar (MEA) several times until pure colonies were obtained. Purified isolates were
61 maintained on MEA slants. The slants were stored at 4°C until use.

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63 **2.4 Screening for Production of endo- β -mannanase**

64 Selective medium ML1 devoid of agar-agar was used to grow the isolates for the production of endo- β -mannanase.
65 The carbon source was replaced with Locust bean gum (LGB) for the purpose of this screening. Elenmeyer flasks (250
66 mL) containing 50 mL of the above culture medium was inoculated with a 5day culture inoculum. The inoculum was a
67 1cm (diameter) agar piece cut out with the aid of a cock-borer from a pre-cultured agar plates. After 5 days of
68 incubation at 30°C, the cultures were harvested by cold centrifugation at 10000 rpm, 4°C for 15 minutes and
69 quantitatively assayed for the activity of endo- β -mannanase.

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71 **2.4.1 Endo- β -mannanase Assay**

72 The assay mixture for endo- β -mannanase activity contained 0.5 mL of 0.5% (w/v) Locust bean gum (LGB) prepared in
73 50 mM sodium citrate buffer, pH 5.0 and 0.5 mL of the culture broth. The reaction mixture was maintained at 50°C for
74 30mins. After incubation, 1 mL of DNS reagent was added. The whole reaction mixture was boiled for 10mins. The
75 development of red-brown colour was measured with spectrophometer (Lamda 25 UV/Vis Spectrophotometer) at 540
76 nm. One unit of enzyme activity (U) is defined as the amount of enzyme liberating 1 μmol of mannose per minute
77 under the assay conditions.

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79 **2.5 Identification of the screened isolate**

80 The Isolate showing remarkable mannanase production ability was selected for identification and further experiments.
81 The cultural, microscopic and molecular characteristic of the selected isolate was examined in other to identify it.

82 **2.6 Morphological Characterization**

83 Purified fungal isolate was transferred to potato dextrose agar plate and incubated for 3 to 5 days in order to observe
84 its cultural characteristics. The cultural characteristics of the isolate were observed with respect to their appearance,
85 colour, and shapes on PDA plates. Furthermore, the cellular morphology of the isolates was also observed. Wet mount

86 preparation of the fungal isolate was made using lactophenol blue according to the method of Fawole and Oso [15].
87 The preparation was then examined with ×40 objective lens.
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89 **2.6 Molecular Characterization**

90 **2.6.1 DNA Extraction**

91 Cells of the selected isolate grown in a broth medium was centrifuged using Thermo scientific Sorvall Lynx 6000 super-
92 speed centrifuge at 10000 rpm for 5 minutes and washed with distilled water. This was then resuspended in a 400 µL
93 solution containing 0.3 mg/mL lyticase and 8 µL/mL β-mercaptoethanol in extraction buffer (1 mol/L sorbitol, 100
94 mmol/L sodium citrate, 60 mmol/L EDTA, pH 7.0), and incubated in a Clifton waterbath (Model: S/W97719) for 3 hrs at
95 37°C. Then, 1 volume of lysis buffer (2% SDS in 50 mmol/L Tris, 10 mmol/L EDTA, pH 8.0) was added and the mixture
96 shaken gently and incubated at room temperature for 10 min after which 200 µL of 5 mol/L NaCl was added. The
97 suspension was maintained in ice for 2 hrs. The pellet was harvested by centrifugation at 13,000 rpm for 10 mins, then
98 suspended in 200 µL of Tris–EDTA buffer after which the DNA was then de-proteinated with a phenol–chloroform–
99 isoamylalcohol mixture (25:24:1). The aqueous layer was collected and DNA in it was precipitated with ethanol (2
100 volumes). It was harvested by centrifugation (13000 rpm for 15 min) and then washed in ice-cold 70% ethanol after
101 which the DNA pellets were dissolved in 60 µL of sterile distilled water.
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105 **2.6.2 PCR amplification and sequencing of the rDNA internal transcribed spacer region (ITS)**

106 The primers used to amplify the rDNA ITS were ITS1 (CGG GAT CCG TAG GTG AAC CTG CGG) and ITS4 (CGG
107 GAT CCT CCG CTT ATT GAT ATG C) as described by White *et al.* [16]. The amplification reaction was done in a 50
108 µL volume containing 20 pmol of each primer, 300 ng of genomic DNA template, 0.25 mmol/L each dNTP, 1.5 mmol/L
109 MgCl₂, and 0.5 U of *Taq* polymerase. The reactions were run for 34 cycles with denaturation at 94°C for 45 s, annealing
110 at 60 °C for 1 min, and extension at 72 °C for 2 min. An initial denaturation during 4 min at 94 °C and a final 5-min
111 extension at 72 °C were used. Amplified products from PCRs were sequenced using automated sequencer (Chromus
112 Biotech, Chennai). The sequence Similarity search was done for the rDNA sequences using online search tool called
113 BLAST (<http://www.ncbi.nlm.nih.gov/blast/>). The unknown organism was identified using the maximum aligned
114 sequence through the BLAST search.
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116 **2.6.3 Storage and Maintenance of Identified isolates**

117 Identified isolate after screening was cultured in PDA slants using MacCartney bottles. They were then stored at 4°C
118 and sub-cultured every 3 to 4 weeks. This isolate has been deposited in the Gene Bank the KR871216 as the
119 accession number.
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121 **2.7 Production characteristic of endo-β-mannanase by *Aspergillus flavus* PT7**

122 The various factors that could affect the production of mannanase were varied in order determine the conditions best
123 suited for the production of this enzyme. Factors under consideration included carbon source, nitrogen source, time of
124 fermentation, size of inoculums and initial moisture content of the substrates.
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126 **2.7.1 Inoculum preparation**

127 After 5 days of cultivation of the fungal isolate at 30°C, the spores were obtained from the slants by shaking them off
128 from the surface of matured their mycelia using 10 mL of sterile distilled water. Total spore count was calculated. 1 mL
129 of the spore suspension was dispensed into a sterile test tube to which 0.1mL of lactophenol blue was added. A sterile
130 syringe was used to introduce the mixture into the Neubauer counting chamber and was counted under x40 objective
131 lens of the microscope. Once initial spore count was obtained, dilution factors were calculated for fermentation needs.
132 In this experiment, spore concentration in fermentation medium was 1×10⁶ spores/mL [17].
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134 **2.7.2 Production of of endo-β-mannanase by *Aspergillus flavus* PT7 from different carbon sources.**

135 The following carbon sources: copra meal, palm kernel cake and soy bean meal (agro-waste) in solid state
136 fermentation experiment and birchwood xylan, locust bean gum, carboxymethyl cellulose, glucose, xylose and
137 arabinose (refined carbons) in a submerged fermentation were examined for their ability to induce the production of
138 endo-β-mannanase.

139 Solid State Fermentation with complex carbon substrates for the production of endo-β-mannanase by
140 *Aspergillus flavus* PT7.

141 In the solid state fermentation experiment, Ten grams of each of the dried carbon source (agro-waste) (dried to a
142 constant weight by oven drying at 60°C) was wetted with ML1 medium (pH 5.0) at 50 % (v/w) [14]. The whole content
143 of the flasks were autoclaved at 121°C for 15min after which they were allowed to cool to room temperature. The
144 cooled substrates were then inoculated with the fungal spores at 4% inoculum level and incubated for 30°C for 72 hrs
145 in a stationary mode. The extraction of the produced enzyme was done by adding 100 mL 50 mM Sodium citrate buffer

146 (pH 5) to the fermented matter. This whole content was then centrifuged at 10000 rpm for 10 minutes. The supernatant
147 was as the crude enzyme preparation. The presence of endo- β -mannanase activities was assayed as previously
148 outlined.

149 **2.7.2.1 Submerged Fermentation of refined carbon substrates for the production of endo- β -mannanase by** 150 ***Aspergillus flavus* PT7.**

151 In submerged fermentation experiment, the ML1 medium (pH 5.0) was supplemented with each of the refined carbon
152 sources at 1% w/v. The whole content of the flasks were autoclaved at 121°C for 15min. The flasks and their contents
153 were allowed to cool to room temperature. The cooled substrates were then inoculated with each of the isolates at 4%
154 (v/w) fungal spores and incubated at 30°C for 7 days in a static or stationary condition. At the end of the fermentation,
155 the whole content of the broth was centrifuged at 10000 rpm for 10 minutes. The supernatant was as the crude
156 enzyme preparation. The presence of endo- β -mannanase activities was assayed as previously outlined.

159 **2.7.3 Effect of Nitrogen sources on the production of endo- β -mannanase by *Aspergillus flavus* PT7.**

160 Following the method of Darah and Omar (2010), eight (8) nitrogen sources of which six (6) were organic (Urea,
161 Peptone, Yeast Extract, Casein, Tryptone, and Soy bean Meal) and two (2) inorganic (KNO₃ and NH₄NO₃) were
162 applied into the solid substrate at the concentration of 4% (w/w) to study their effect on the quantity of endo- β -
163 mannanase produced the fungal isolate. Moisture content was kept at 50%, pH 5.0 and incubation was done at 30°C
164 for 7 days.

166 **2.7.4 Test of Environmental factors on production of endo- β -mannanase by *Aspergillus flavus* PT7.**

167 In these series of experiments, the cheap agro-waste supporting the production of Mannanase best was used as the
168 main carbon source in solid state fermentation.

169 **2.7.4.1 Effect of initial pH on the production of endo- β -mannanase by *Aspergillus flavus* PT7.**

170 The effect of different pH levels on the production of endo- β -mannanase was done by adjusting the moisture content of
171 substrate with buffered basal medium of varying pH (3.0, 4.0, 5.0, 6.0 and 7.0). The buffers used included 50mM
172 Sodium citrate buffer (pH 3.5-6.0) and 50mM Sodium phosphate buffer (pH 6.0-7.0). Sterilization was done at 121°C
173 for 15 minutes before inoculating with 2% (v/w) fungal spores. The setup was incubated for 7 days at 30°C.

175 **2.7.4.2 Effect of moisture content on the production of endo- β -mannanase by *Aspergillus flavus* PT7.**

176 The effect of the moisture content of the substrate on the enzyme production was determined at five different moisture
177 levels (50, 75, 100, 125 and 150%; v/w) prepared by the addition of basal medium to the substrates prior to
178 sterilization. Thereafter, the set up was inoculated with 4% (v/w) inoculum and incubated for 7 days at 30°C. The pH of
179 basal medium was kept at 5.0 with sodium citrate buffer.

181 **2.7.4.3 Effect of inoculum size on the production of endo- β -mannanase by *Aspergillus flavus* PT7.**

182 The effects of different sizes of inocula on the production of endo- β -mannanase were studied by inoculating the
183 sterilized buffered substrates (50 mM sodium citrate pH 5.0) with 1%, 2%, 4%, 8% and 10 %, (v/w) spore solutions.
184 The inoculum was prepared as described previously. One milli Litre (1 mL) of the inoculum contained 1x10⁶ spores/mL.
185 The set up was incubated at 30°C for 7 days.

188 **2.7.4.4 Effect temperature on the production of endo- β -mannanase by *Aspergillus flavus* PT7.**

189 Four different incubation temperatures- 27°C 30°C, 35°C, and 40°C- were used to cultivate the cultures for endo- β -
190 mannanase synthesis according to the method of Rashid *et al.* [18] so as to study the effect of temperature on the
191 production of this enzyme by *Aspergillus flavus* PT7.

194 **2.7.4.5 Effect of incubation time on the production of endo- β -mannanase by *Aspergillus flavus* PT7.**

195 The time course of fermentation on endo- β -mannanase production was studied by assaying for the amount of each of
196 the enzymes produced at 3, 5, 7, 10 and 14 days in the crude enzyme filtrate taken at this respective time during
197 fermentation. The pH of the fermentation medium was kept at 5.0 and incubation was done at 30°C.

199 **2.7.5 Regulation of the production of endo- β -mannanase by *Aspergillus flavus* PT7.**

200 The effect of the presence of easily utilizable sugars as supplements on the production of the endo-mannanase was
201 studied. The carbohydrates used were glucose, galactose, arabinose and xylose. The fermentation setup was
202 supplemented with 2% (w/w) of these simple sugars singly. It was then incubated at 30°C for 7 days, after which the
203 enzymes produced were harvested, assayed and the results compared to the amount of enzymes produced in the
204 absence of these simple sugars [19].

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3. RESULTS AND DISCUSSION

A total of 38 moulds were isolated from degraded palm kernel cake (PKC) and potato peels (PT). The isolate with remarkable ability to produce mannanase enzymes was identified. The identification was done after cultural, morphological and molecular examination of the selected isolates.

The isolate designated as PT7 was the best producer of mannanase with enzyme activity of 2.11 ± 0.21 U/mL on submerged fermentation. It appears greenish on culture medium; has septate hypha with long conidiospores. The conidial heads are radiate in shape. It was molecularly confirmed to be *Aspergillus flavus*. As illustrated in an un-rooted dendrogram constructed using a neighbour joining tree model (Figure 1) *Aspergillus flavus* PT7 is closely related to *Aspergillus* sp BAB-3401. This isolate has been deposited in the Gene Bank the KR871216 as the accession number.

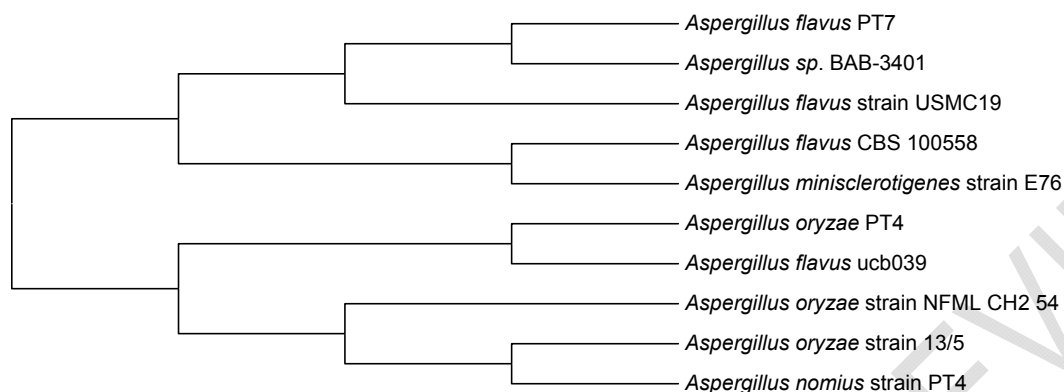


Figure 1: The phylogenetic tree of *Aspergillus flavus* PT7 based on the 18S rRNA sequence comparison of related isolates. The evolutionary history was inferred using the Neighbor-Joining method. The percentage of replicate trees in which the associated taxa clustered together in the bootstrap test (500 replicates) are shown next to the branches. Evolutionary analyses were conducted in MEGA6.

3.1 Effect of different carbon sources on the Production of endo- β -mannanase by *Aspergillus flavus* PT7.

Mannanase was best produced in the presence of locust bean gum with enzyme activity of 97.35 ± 1.18 U/gds. Copra meal was the second best inducer of this enzyme with an activity of 85.86 ± 3.93 U/gds. This was followed by xylan and CMC with 45.07 ± 4.12 U/gds and 45.97 ± 0.08 U/gds enzyme activity respectively. Production in the presence of soybean meal, PKC, xylose, arabinose and glucose was generally low with the least value of 10.41 ± 1.14 U/gds recorded for glucose (Table 1).

The isolate was able to grow and produce mannanase on all cheap agro-waste (carbon sources) tried out although in varying quantities. The variations in the ability of these carbon sources to support mannanase production in *A. niger* PT4 can be attributed to the composition of carbohydrates in these substrates as well as their nutritional contents [20, 19]. Copra meal, of all the cheap agro-waste used as carbon source was the best inducer of mannanase production in the isolate. The proximate composition analysis of CM in the cause of this work revealed that CM has higher protein and moisture content than PKC, thus its ability to support the growth of the isolate and allowed higher enzymes production.

3.2 Effect of different Nitrogen sources on the production of endo- β -mannanase by *Aspergillus flavus* PT7.

The effect of different nitrogen sources on the production of mannan-degrading enzymes using the best supporting complex carbon source for each enzyme in a solid state fermentation was experimented. The nitrogen sources tried out included peptone, yeast extract, urea, casein, soybean meal, and tryptone (organic nitrogen sources); others included KNO_3 and $(\text{NH}_4)_2\text{SO}_4$ (inorganic nitrogen sources) (Table 2).

Table 1: Production the Production of endo- β -mannanase by *Aspergillus flavus* PT7 using different carbon sources in a solid state fermentation at 50% moisture level.

Substrates	Mannanase Activity (U/gds)
Soy-Bean meal	33.44 ± 0.48^d
Copra meal	85.86 ± 3.93^b
PKC	35.86 ± 0.40^d

Xylan	45.07±4.12 ^c
CMC	45.97±0.08 ^c
LBG	97.35±1.18^a
Xylose	31.31±4.16 ^{de}
Arabinose	24.86±0.34 ^e
Glucose	10.41±1.14 ^f

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The carbon source used in the production of the enzyme (copra meal), just like PKC has high protein content; about 15-20% crude protein (Sundu and Dingle 2003). This is enough to support growth and enzyme production on from isolate. This is similar to observation of Marouk and El Ahwany [19] that omitting nitrogen source from the growth medium of *Bacillus amyloliquefaciens* when potato peel was the sole carbon source resulted in the production of high quantities of mannanase. This indicates that some lingo-cellulosic material can serve as carbon and nitrogen source.

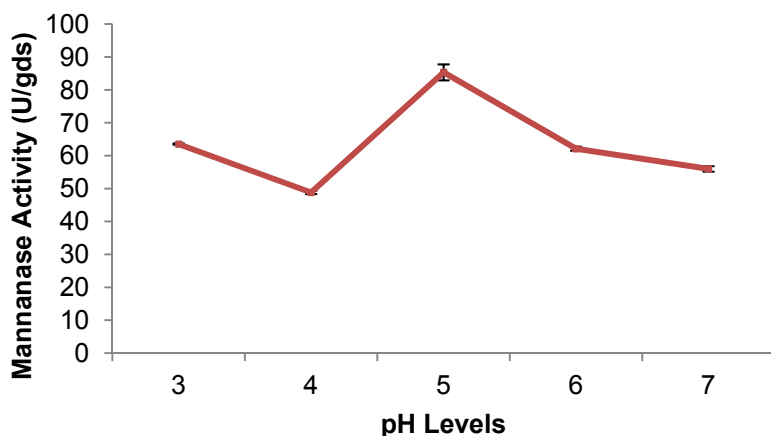
3.3 Effect of pH on the Production of endo-β-mannanase by *Aspergillus flavus* PT7.

The influence of initial pH of the culture medium on the endo-β-mannanase production was investigated within the pH range of 3.0 to 7.0 (Figure 2). The pH of the medium used was regulated by wetting the substrates with a basal medium prepared in appropriate buffer. Mannanase production from *A. flavus* PT7 was highest at pH 5.0 with enzyme activity of 85.31±2.43 U/gds.

Table 2: Effect of different nitrogen sources on production of endo-β-mannanase using the best supporting complex carbon source for individual enzyme in a solid state fermentation at 50% moisture level.

Nitrogen Sources (0.4g/g)	Mannanase Activity (U/gds)
Peptone	71.02±1.17 ^c
Yeast Extract	63.71±0.61 ^d
Urea	43.30±1.58 ^f
KNO ₃	77.96±0.87 ^c
Casein	63.06±3.31 ^d
Soybean Meal	41.91±0.20 ^f
Tryptone	69.88±0.53 ^c
Ammonium Sulphate	49.43±0.87 ^e
Control	94.54±0.42^a

There was a gradual decrease in mannanase activity at pH 6.0 and 7.0 with enzyme activities of 62.11±0.59 and 55.97±0.83 U/gds respectively. The optimum pH 5.0 for mannanase production is similar to that reported by [21, 22]. Kote *et al.* [21] and Chantorn *et al.* [22] reported maximum production of mannanase from *Aspergillus flavus* and *Penicillium oxalicum* KUB-SN2-1 grown in a fermentation medium having an initial pH at 5.0 respectively.



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290 **Figure 2: Effect of initial pH on the production of endo-β-mannanase using the best carbon and nitrogen**
291 **sources in a solid state fermentation at 50% moisture level.**

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295 **3.4 Effect of different moisture levels on the production of endo-β-mannanase by *Aspergillus flavus***
296 **PT7.**

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298 Table 3 shows the effect of moisture content on the production of mannanase by the fungi isolate. The moisture
299 content of the substrates was adjusted at different ratios between the substrates and the basal medium added. The
300 basal medium was prepared by dissolving appropriate salts and nitrogen sources in buffers.

301 Production of mannanase by *A. flavus* PT7 was not significantly different at 50 and 75% (v/w) moisture with 87.28±0.42
302 and 82.62±14.10 U/gds. At 100% (v/w), highest production of cellulase was reached (124.32±10.79 U/gds). There was
303 a sharp decrease in enzyme production at higher moisture levels of 125 and 150 % (v/w).

304 In solid state fermentation for the production of microbial metabolites, moisture plays a very vital role and drastically
305 influences the fermentation process [23]. Depending on the substrate used and the organism too, moisture demand
306 could be as low as 50 % (v/w) and as high as 150 % (v/w). This variation could be as a result of difference in the rate of
307 water absorption by different substrates [23]. Water causes the swelling of substrate thus enhancing good utilization of
308 substrates by microorganisms.

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310 **Table 3. Effect of moisture content on the production of endo-β-mannanase in solid state fermentation**
311 **incubated at 30°C for 7days**

Moisture (% v/w)	Mannanase Activity (U/gds)
50	87.28±0.42 ^b
75	82.62±14.10 ^{bc}
100	124.32±10.79^a
125	65.55±0.58 ^{bc}
150	57.98±4.38 ^c

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316 **3.5 Effect of different inoculum sizes on the production of endo-β-mannanase by *Aspergillus flavus***
317 **PT7.**

318 Inoculum sizes based on standardized number of spores having 1×10⁶ spores/ml were examined using spore
319 concentration of 1, 2, 4 8 and 10% (v/w) of dry substrates. It was found out that increase in inoculum size led to
320 increase in enzyme production (Table 4). Production of mannanase was optimum at 8% (v/w) inoculum size with an
321 activity of 128.56±0.42 U/gds, however this activity was not significantly different from the 120.54 ±10.77 recorded at
322 4% (v/w) inoculum size. At 10% (v/w) inoculum size, production dropped drastically to 56.96±8.20 U/gds. Mannanase
323 production at 2% (v/w) and 10% (v/w) inoculum sizes though not significantly different, but they were the lowest.

324 Determining the optimum density of microorganism for enzyme production in solid state fermentation is very important
325 if best production conditions must be met. Inoculum size below optimum will affect the time needed for cells to
326 proliferate, colonize and utilize the substrate and produce the desired products [24]. At the other extreme, higher

327 inoculum density above optimum has been generally observed to affect enzyme production adversely [25]. This can be
328 correlated to the fact that too much microbial biomass is produced as a result of higher inoculum thus leading to
329 depletion of nutrient in shorter time without adequate metabolite production [26].
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331 **Table 4: Effect of inoculum size (% v/w) on production of endo- β -mannanase in solid state fermentation**
332 **incubated at 30°C for 7days using the best moisture level of 100% (v/w).**
333

Inoculum size (%)	Mannanase Activity (U/gds)
1	12.39±0.40 ^c
2	46.30±0.64 ^b
4	120.54±10.77^a
8	128.56±0.42^a
10	56.96±8.20 ^b

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344 **3.6 Effect of different incubation temperature on the production of endo- β -mannanase by**
345 ***Aspergillus flavus* PT7.**
346

347 The effect of incubation temperature on mannanase production by the fungal isolate was examined. Mannanase
348 production was highest at 30°C. Production at 27°C and 35°C were not significantly different. The highest activities
349 recorded for this enzyme was 158.52±10.99. There was a gradually reduction in the quantities of enzymes produced
350 from 35°C to 40°C (Table 5).

351 This is in line with the observations of other authors [27-29]. Enzymes production at this temperature is applauded
352 because it is still within room temperature thus energy cost can be saved. According to Manpreet *et al.* [30], solid
353 states fermentation is better operated within the mesophilic range because most of the microorganism used in the solid
354 state fermentation are mesophilic having their optimum growth between 20°C and 40°C. Furthermore, a higher
355 temperature above this could lead to drying up of the available water thus reducing the moisture concentration in the
356 substrates that would have been used by microorganisms for growth and metabolite production.
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360 **Table 5: Effect of incubation temperature on production of endo- β -mannanase in solid state fermentation**
361 **incubated for 7days using the best moisture levels and inoculum sizes (8% (v/w)).**
362

Temperature (°C)	Mannanase Activity (U/gds)
27	100.43±0.19 ^b
30	153.24±5.69^a
35	104.23±0.34 ^b
40	40.06±3.70 ^c

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365 **3.7 Effect of incubation time on the production of endo- β -mannanase by *Aspergillus flavus* PT7.**
366

367 Table 6 shows the production of mannanase enzyme between 4 to 18 days of cultivation. Samples were taken at 3 and
368 4 days intervals and assayed for the quantity of enzyme produced. Production of mannanase increased from
369 130.23±0.021 U/gds on day 4 to reach a peak on day 7 with 170.34±4.35 U/gds. In subsequent days, there was a
370 gradual reduction in the amount of enzyme produced. Production at day 10 and 14 were not significantly different. The
371 least value of 62.62±6.16 U/gds was recorded on day 18. Wanderly *et al.* [31] asserted that the incubation time for
372 enzyme production by microorganisms depends on the nutrients present in their growth medium as well as other
373 cultural conditions. According to Jahangeer *et al.* [32], the kinetics of enzyme production by most fungal isolates is
374 observed to be highest after 7 days and production declines after 10 days of incubation. This decline in enzyme
375 production is usually as a result of decline in the available nutrient for growth and enzyme production.
376

377 **Table 6: Effect of incubation temperature on the production of endo- β -mannanase in solid state fermentation**
378 **incubated for 7days using the best moisture levels and inoculum sizes (8% (v/w)).**
379

Incubation Time (days)	Mannanase Activity (U/gds)
4	130.23±0.21 ^b
7	170.34±4.35^a
10	117.71±0.10 ^c
14	113.63±0.21 ^c
18	62.62±6.16 ^d

4.8 Repressive and Inductive effects of simple sugars on the production of endo-β-mannanase by *Aspergillus flavus* PT7.

Addition of various carbohydrates at 0.2 g/g in the production medium containing CM as substrates in order to evaluate their inductive/repressive effect on the production of mannanase enzymes was tested (Table 7). The sugars used included glucose, galactose, xylose and arabinose. There was a severe inhibitory effect associated with the addition of simpler and easily utilizable carbohydrates on the production of mannanase. Highest repressive effect on mannanase production was in the presence of glucose (92.0.17±0.06 U/gds). Production of mannanase (of which mannanase is one) by microorganisms has largely been found to be inducible [33]. Similar trend was observed by Sachslehner *et al.* [34] and Mabrouk and El-Ahwany [19] in the production of mannan-degrading enzymes from *Sclerotium rolfsii* and *Bacillus amyloliquefaciens* respectively. They both reported inhibition in the production of mannan-degrading enzymes in these organisms in the presence of easily utilizable glucose monomers.

Table 7. Repressive and Inductive effects of simple sugars (0.2 g/g) on the production of endo-β-mannanase in a solid state fermentation.

Sugars (0.2 g/g)	Mannanase Activity (U/gds)
control	170.01±0.14^a
Glucose	92.17±0.06 ^c
Galactose	95.21±0.10 ^b
Arabinose	91.01±1.22 ^c
Xylose	95.37±0.30 ^b

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COMPETING INTERESTS

Authors have declared that no competing interests exist.

REFERENCES

- Girio, FM, Fonseca, C, Carvalheiro, F, Durate, LC, Marques, S and Bogel-Lukasik, R. Hemicelluloses for fuel ethanol.: a review. *Bioresources Technology*, 2010; **13**: 4775-4800.
- Reid JSG, Edwards ME, Dickson CA, Scott C and Gidley, MJ. Tobacco transgenic lines that express fenugreek galactomannan galactosyltransferase constitutively have structurally altered galactomannans in their seed endosperm cell walls. *Plant Physiology*, 2003;**131**: 1487–1495.
- Petkowicz CLO, Reicher F, Chanzy H, Taravel FR and Vuoug R. Linear Mannan in the endosperm of *Schizolobium amazonicum*. *Carbohydrate Polymer*, 2001;44: 107-112.
- Dhawan S and Kaur J. Microbial mannanases: an overview of production and applications. *Critical Reviews in Biotechnology*, 2007;**27**: 197–216.
- Talbot G and Sygusch J. Purification and characterization of thermostable β-mannanase and α-galactosidase from *Bacillus stearothermophilus*. *Applied Environmental Microbiology*, 1990;**56**: 3505-3510.
- Takahashi R, Kusakabe L, Maekawa A, Suzuki T and Murakami K. Some properties of extracellular mannanase. *Japanese Journal of Tropical Agriculture*, 1983;**27**:140.

- 424 7. Zakaria MM, Yamamoto, S and Yagi T. Purification and characterization of an endo-1, 4- β -mannanase from
425 *Bacillus subtilis* KU-1. *FEMS Microbiol Lett* 1998;158, 25-31.
- 426 8. Sachslehner A and Haltrich D. Purification and some properties of a thermostable acidic endo-1,4- β -
427 mannanase from *Sclerotium (Athelia) rolfsii*. *Universität für Bodenkultur (BOKU), Austria*. 1999;177: 47-55.
- 428 9. Kurakake M and Komaki T Production of β -mannanase and β -mannosidase from *Aspergillus awamori* K4 and
429 their properties. *Current Microbiology*, 2001;42:377–380.
- 430 10. Ferreira HM and Filho EXF. Purification and characterization of a mannanase from *Trichoderma harzianum*
431 strain T4, *Carbohydr Polym*, 2004;57:23-29.
- 432 11. Ademark P, Larsson M, Tjerneld F, and Stålbrand H. Multiple galactosidases from *Aspergillus niger*:
433 purification, characterization and substratem specificities. *Enzyme and Microbial Technology*. 2001;29:441-
434 448.
- 435 12. Zhang J, He, ZM, and Hu K. Purification and characterization of β -mannanase from *Bacillus licheniformis* for
436 industrial use. *Biotechnol Lett* 2000; 22:1375-1378.
- 437 13. Haung XP and Monk C. Purification and characterization of a cellulase from a newly isolated thermophilic
438 aerobic bacterium *Caldibacillus cellulovorans* gen. nov.sp. *World Journal of Microbiology and Biotechnology*,
439 2004;20: 85-92.
- 440 14. Santiago SDN, Gonzalez CR, Almendarez BG, Fernandez FJ, Jurado AT and Ochoa SH. Physiology,
441 morphological, and mannanase production studies on *Aspergillus niger* UAM-GS mutants. *Electronic Journal*
442 *of Biotechnology*, 2007;9: 1.
- 443 15. Fawole MO and Oso BA. *Laboratory Manual of Microbiology*. Spectrum Books Ltd., Ibadan, Nigeria, pp: 1-48.
444 2004
- 445 16. White TJ, Bruns T, Lee S and Taylor J. Amplification and direct sequencing of fungal ribosomal RNA genes
446 for phylogenetics. In: *PCR protocols:A guide to methods and applications*. Edited by M.A. Inns, D. H. Gelfrand,
447 J. J. Sninsky, and T. J. Withe. Academic Press, New York. pp. 315–322. 1990
- 448 17. Sae-Lee N. The production of fungal mannanase, cellulose and xylanase using palm kernel meal as a
449 substrate. *Walailak Journal of Science and Technology*, 2007;4: 67-82.
- 450 18. Rashid SA, Ibrahim D and Omar IC. Mannanase production by *Aspergillus niger* USM F4 via solid substrate
451 fermentation in a shallow tray using palm kernel cake as a substrate. *Malaysian Journal of Microbiology*, 2012;
452 8(4): 273-279.
- 453 19. Mabrouk MEM and El Ahway AMD. Production of β -mannanase by *Bacillus amylolequifaciens* 10A1 cultured
454 on potato peels. *African Journal of Biotechnology* 2008; 7(8):1123-1128.
- 455 20. Chantorn ST, Buengsisawat K, Pokeseam A, Sombat T, Dangpram P, Jantawon K, Nitisinprasert S.
456 Optimization of extracellular mannanase production from *Penicillium oxalicum* KUB-SN2-1 and application for
457 hydrolysis property. *Songklanakarin Journal of Science and Technology*, 2013;35(1):17-22
- 458 21. Kote NV, Patil AG, Mulimani VH. Optimization of the production of thermostable endo-beta-1,4 mannanases
459 from a newly isolated *Aspergillus niger* gr and *Aspergillus flavus* gr. *Applied Biochemistry and*
460 *Biotechnology*, 2009; 152(2):213-223.
- 461 22. Pandey A. Solid-state fermentation. *Biochemical Engineering Journal*, 2003;13: 81–84.
- 462 23. Ramachandran S, Patel AK, Nampoothiri KM, Francis F, Nagy V, Szackacs G, Pandey A. Coconut oil cake-a
463 potential material for production of α -amylase. *Bioresource Technology*, 2004;93(2): 169-174.
- 464 24. Ibrahim D, Puspitaloka H, Rahim RA and Hong LS () Characterization of Solid State Fermentation Culture
465 Conditions for Growth and Mananase Production by *Aspergillus niger* USM F4 on Rice Husk in Tray System.
466 *British Biotechnology Journal*, 2012;2(3):133-145.
- 467 25. Kumar RS, Shankar T and Anandapandian KTK. Characterization of alcohol resistant yeast *Saccharomyces*
468 *cerevisiae* isolated from Toddy. *International Research Journal of Microbiology*, 2011;2(10): 399-405.
- 469 26. De Ioannes P, Peirano A, Steiner J and Eyzaguirre J () An α -L-arabinofuranosidase from *Penicillium*
470 *purpurogenum*: production, purification and properties. *J Biotechnol* 2000;76:253–258.
- 471 27. Koseki T, Miwa Y, Mese Y, Miyanaga A, Fushinobu S, Wakgi T, Shoun H, Matsuzawa H and Hashizume K.
472 Mutational analysis of N-glycosylation recognition sites on the biochemical properties of *Aspergillus kawachii*
473 α -L-arabinofuranosidase 54. *Biochimica et Biophysica Acta (BBA)*, 1760(9): 1458 – 1464.
- 474 28. Fritz M, Ravanal MC, Braet C and Eyzaguirre J (2008) A family 51 α -L-arabinofuranosidase from *Penicillium*
475 *purpurogenum*: purification, properties and amino acid sequence. *Mycologia Research*, 112(8): 933– 942.
- 476 29. Manpreet S, Sarwat S, Sachi D, Pankaj S and Banerjee UC. Influence of Process Parameters on the
477 Production of Metabolites in Solid-State Fermentation. *Malaysian Journal of Microbiology* 2005;1(2): 1-9
- 478 30. Wanderley KJ, Torres FAG, Moraes LMP and Ulhoa CJ. Biochemical characterization of α -amylase from the
479 yeast *Cryptococcus flavus*. *FEMS Microbiology Letters*, 2004;231(2):165–169
- 480 31. Jahangeer S, Khan N, Jahangeer S, Sohail M, Shahzad S, Ahmad A, Ahmed Khan S. Screening and
481 characterisation of fungal cellulases isolated from the native environmental source. *Pakistan Journal of Botany*,
482 2005;37(3): 739-748.

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32. Singh C, Ahuja N, Batish M, Capalash N, Sharma P. Biobleaching of wheat straw-rich-soda-pulp with alkalophilic laccase from γ -*Proteobacterium* JB: Optimization of process parameters using response surface methodology. *Bioresource Technology*, 2003;**99**:7472-7479.
33. Sachslehner A, Haltrich D, Nidetzky B, Kulbe KD. Production of Hemicellulose and cellulose-degrading enzymes by various strains of *Sclerotium rolfsii*. *Applied Biochemistry and Biotechnology*, 1997;**63-65**:189-201.

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