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3 **Optimization of process parameters for the treatment of Crude oil spill polluted**  
4 **water surface by sorption technique using fatty acid grafted ogbono shell as a**  
5 **sorbent**

6 **ABSTRACT**

7 This work focuses on the optimization of the adsorption technique using fatty acid grafted  
8 ogbono shell for the removal oil from polluted water surface. The shell was carbonized at a  
9 temperature of 600°C for 4hours and then further modified with stearic acid. The surface  
10 morphology of raw and grafted ogbono shell was studied Scan Electron microscope (SEM) while  
11 Fourier Transform Infra-red Spectroscopy (FTIR) was used to investigated the functional group  
12 of different minerals. Proximate analysis was carried out to determine the surface area of the  
13 agro wastes before and after modification. The process parameters were optimized using  
14 response surface methodology. Physiochemical characterization of the adsorbents showed that  
15 surface area increased significantly after carbonization and modification. SEM and FTIR results  
16 revealed that more micro porous surfaces were created on the surface of the adsorbent after  
17 modification. The optimum time, temperature, dosage, pH and percentage oil removal were;  
18 Time of 10mins, temperature of 60°C, dosage of 1.4g, pH of 3 at the theoretical percentage  
19 removal of 78.77%

20 Key words: Optimization, ogbono shell, crude oil, adsorption

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**INTRODUCTION**

23 Crude oil is a combustible liquid found in the earth's sedimentary mantle and is basically  
24 composed of a complex mixture of hydrocarbons with its color ranging from brown to almost  
25 black depending on the content and structure of the resinous substances it contains (Uzoije et al.,  
26 2011). Over the years, crude oil spill and its concomitant pollution have been in front burner in  
27 environmental issues over the world and in particular the rich Niger Delta of Nigeria (Uzoije et  
28 al., 2011). Crude oil spillage results when oil has been released into the environment (Ali et al.,  
29 2012). The oil spills in seawater and soil are usually as a result of exploration or transportation or  
30 storage activities (Annunciado et al., 2005; Baars, 2002). Spillage is broadly categorized into  
31 four groups, namely minor, medium, major and disaster (Banerjee, 2006). The most frequent of

32 these is the minor spillage which is oil discharge less than 25 barrels in land waters or less than  
33 250 barrels on land, offshore and coastal water (Behnood et al., 2013). This category of spill  
34 contributes more to the total volume of annual spillage than other categories (Chung et al., 2011).

35 Clean-up is necessary after a spill for the protection of the environment and human health. In  
36 control of spillages, a wide range of tool and techniques are used to clean oil spills. Among the  
37 techniques include; chemical remediation, bioremediation, phytoremediation, thermal  
38 desorption, adsorption and land fill in the case of soil spillage. Adsorption technique is of great  
39 interest due to its cheapness and convenience (Sayed et al., 2003). Natural sorbents and varieties  
40 of organic vegetable waste products, such as peat moss, wood, cotton, rice straw, corncobs and  
41 kapokshave been recently gained an appraisal both internationally and locally as an effective  
42 sorbents in oil spill treatment (Nwadiogbu et al., 2016; Choi and Cloud, 1992; Deschamop et al.,  
43 2003) These agro wastes are at no cost and available locally. Optimization of the process  
44 parameters was done in this work using response surface methodology (RSM). Response surface  
45 methodology is a statistical tool designed specifically for optimization studies. Its usage depicts  
46 the effect of independent factors on the results or expected results. The input elements or factors  
47 are the independent variables while the response(s) or the outputs are the dependent variables  
48 (Datta, 2011). RSM relates item properties by utilizing regression equation that portrays  
49 interrelations between information factors and item properties (Adeyanju et al., 2016). The most  
50 often used type of RSM is central composite design (CCD) and Box Behnken design (BBD).  
51 Therefore, the aim of this study is to optimize the use of esterified ogbono shell (agro wastes) as  
52 an adsorbent in the remediation of crude oil layer polluted water surface using Box Behnken  
53 design.

## 54 **Materials and method**

### 55 **Materials**

56 The major raw material (Ogbono shells) was collected from Akpoga Nike in Enugu State  
57 Nigeria. The shells were first washed and dried under the sun for one week. After which, the  
58 shells were grounded using a commercial grinder at Oye Market in Emene, Enugu State Nigeria.  
59 Other materials used included; Crude oil, distilled water, sodium hydroxide (NaOH), H<sub>2</sub>SO<sub>4</sub>,  
60 HCL, Sieving net, stearic acid, n-hexane.

## 61 **Methods**

### 62 **Preparation of Carbonized Adsorbent (Ogbono Shells)**

63 The dried biomass (Ogbono shells) was carbonized in a muffle furnace at 600°C for 4 hours  
64 respectively. After the carbonization, the samples were cooled and stored in dry transparent  
65 containers for further use (Angelova et al., 2011).

### 66 **Activation of the carbonized ogbono shell by Esterification**

67 Carbonized samples of the biomass (ogbono shell) were treated differently with 0.5g of fatty acid  
68 (stearic acid) in 200ml of n-hexane containing two drops of concentrated H<sub>2</sub>SO<sub>4</sub> as catalyst. The  
69 mixture was refluxed in dean stark apparatus at 65± 2°C for 4 hrs. After reaction, the esterified  
70 acid-grafted ogbono shells were washed severally with n- hexane. The fatty acid grafted biomass  
71 was oven dried at 110°C for 12hrs respectively (Banerjee et al., 2006). They were then kept in  
72 dry tightly closed bottles respectively.

73

74 . They were then kept in dry tightly closed bottle for further use.

75

$$76 \quad \text{Weight percentage gain} = \frac{\text{Weight gain}}{\text{Original weight}} \times 100 \quad (1)$$

### 77 **Characterization of the raw and modified biomass**

78 The surface morphology of the (raw and modified) biomass was studied using Model 302  
79 Hitachi High Field Emission Scanning Electron Microscope and the images at 1mm and 150  
80 magnifications. The method employed by Nwabanne and Igbokwe (2008) was adopted to carry  
81 out Fourier Transformed Infrared analysis of raw and modified biomass (Ogbono shell) using  
82 BUCK model 500 M infrared spectrophotometer. The sample was prepared using KBr and the  
83 analysis was done by scanning the sample through a wave number range of 500 to 4000 cm<sup>-1</sup>.  
84 The proximate analysis parameters and the method of analysis were according to the American  
85 Society for Testing and Materials (ASTMD 5142, 3174, 872 and 3175 for moisture, ash, volatile  
86 and fixed carbon respectively) (Diadem, 2012)

### 87 **Adsorption Experiment**

88 The sorption of crude oil contaminated water was carried out following the method described by  
89 Banerjee et al. (2006). Exactly 50ml of water was measured inside a 100ml beaker. A certain

90 amount of crude oil (0.1-1.4g) depending on the oil/water ratio for a particular run was added  
91 into the beaker. The oil/water mixture was manually stirred for at varying minutes to ensure  
92 proper dispersion of the oil in water. 0.2g of the modified adsorbent was weighed into the  
93 beaker. The beaker containing the sorbent, oil and water was put into a water bath at a varying  
94 temperature. The mixture was stirred for a period of time, depending on the particular run. After  
95 which the mixture was filtered through a net of approximately 250µm. The weight of the net  
96 before and after the filtration was recorded. Meanwhile, the net after the filtration was allowed to  
97 stay for 24hours before the final weight was taken.

98 Percentage removal was also calculated according to the equation below

$$99 \quad \% \text{ removal} = \frac{(C_o - C_e)}{C_o} \times 100 \quad (2)$$

$$100 \quad q_e = \frac{(C_o - C_e)}{M} V \quad (3)$$

101  $C_o$  = Initial oil concentration (mg/l)

102  $C_e$  = Equilibrium Concentration oil at certain time

103  $Q_e$  = Equilibrium adsorption in (mg/g)

104  $V$  = Volume of the aqueous mixture in  $\text{cm}^3$

105  $M$  = Mass of the activated biomass (Esterified ogbono shell) in (g)

### 106 **BBD Design of Experiment using RSM**

107 The sorption of the crude oil layers by activated ogbono shell was optimized using Box Benken  
108 design (BBD) and RMS methods. The independent variables studied were Time  $X_1$  (mins),  
109 temperature  $X_2$  ( $^{\circ}\text{C}$ ), adsorbent dosage  $X_3$  (g), and pH  $X_4$ . The time range of 10 to 60 minutes,  
110 the temperature range of 30 to 70  $^{\circ}\text{C}$ , dosage range of 0.2 to 1.4 and pH range of 3 to 11 were  
111 selected. The coded and uncoded levels of these independent variables are shown in Table 1. The  
112 experimental design was based on BBD. This was done to determine the best conditions for  
113 optimum sorption of the oil onto activated biomass. Equally, this helps to examine the interactive  
114 effects of the four important factors (Time, Temperature, dosage and pH). These factors were the  
115 independent variables while the percentage of oil adsorbed or removed (%R) were the dependent

116 variables or responses. Using the Box Benkhen design (a statistical package in Minitab software  
 117 version 17.1.0) involves varying the independent variables at three different levels (-1, 0, +1). In  
 118 this work, a set of 27 experiments were performed. Table 2 shows the run order, variable  
 119 conditions and the columns for the experimental, predicted and residual values of the oil layer  
 120 sorption unto activated biomass.

121 Table 1: Independent variables with three different levels

Variables	Symbol	Level		
		Low	Centre	High
Time (mins)	X <sub>1</sub>	10	35	60
Temperature (°C)	X <sub>2</sub>	30	60	90
Dosage (w:w)	X <sub>3</sub>	0.2	0.8	1.4
pH	X <sub>4</sub>	3	7	11

122

123

124 Table 2: Design matrix with responses for the sorption of oil from surface water onto  
 125 Esterified Ogbono shell

126

Std	Run	Time: X <sub>1</sub> mins	Temp:X <sub>2</sub> °C	Dosage:X <sub>3</sub> g	pH:X <sub>4</sub>	Coded values				%Sorption Experiment al	%Sorption Predicted	
						X <sub>1</sub>	X <sub>2</sub>	X <sub>3</sub>	X <sub>4</sub>			
5	1	35	60	0.2	3	1	0	0	-1	-1	21.34	23.56
13	2	35	30	0.2	7	1	0	-1	-1	0	36.10	32.56
20	3	60	60	1.4	7	1	1	0	1	0	27.30	23.11
9	4	10	60	0.8	3	1	-1	0	0	-1	28.90	30.12
1	5	10	30	0.8	7	1	-1	-1	0	0	55.75	56.22
10	6	60	60	0.8	3	1	1	0	0	-1	17.30	17.00
3	7	10	90	0.8	7	1	-1	1	0	0	26.34	23.66
14	8	35	90	0.2	7	1	0	1	-1	0	26.11	26.77
7	9	35	60	0.2	11	1	0	0	-1	1	21.88	21.34
24	10	35	90	0.8	11	1	0	1	0	1	29.55	28.97
12	11	60	60	0.8	11	1	1	0	0	1	14.20	14.79
26	12	35	60	0.8	7	1	0	0	0	0	28.07	29.66
16	13	35	90	1.4	7	1	0	1	1	0	26.11	26.78
21	14	35	30	0.8	3	1	0	-1	0	-1	37.23	36.97
19	15	10	60	1.4	7	1	-1	0	1	0	76.40	78.77
2	16	60	30	0.8	7	1	1	-1	0	0	15.80	16.34
25	17	35	60	0.8	7	1	0	0	0	0	24.80	29.66
11	18	10	60	0.8	11	1	-1	0	0	1	30.45	27.89
22	19	35	90	0.8	3	1	0	1	0	-1	12.33	10.14
18	20	60	60	0.2	7	1	1	0	-1	0	22.55	23.11
8	21	35	60	1.4	11	1	0	0	1	1	19.60	21.34
4	22	60	90	0.8	7	1	1	1	0	0	29.40	29.89
23	23	35	30	0.8	11	1	0	-1	0	1	12.34	13.70

6	24	35	60	1.4	3	1	0	0	1	-1	24.23	23.56
15	25	35	30	1.4	7	1	0	-1	1	0	61.67	62.56
17	26	10	60	0.2	7	1	-1	0	-1	0	32.33	36.22
27	27	35	60	0.8	7	1	0	0	0	0	31.23	29.66

127

## 128 Results and Discussion

### 129 Proximate analysis of the raw and modified biomass

130 The characteristics of raw and modified biomass were shown in Table 3. From the Table, it can  
 131 be seen that the raw biomass (ogbono shell) have low fixed carbon, surface area and high volatile  
 132 content and as such suggest that the sample requires activation. Increase in fixed carbon and  
 133 reduction in volatile matter of the activated biomass shows that activation improved the surface  
 134 area of the biomass for adsorption. As observed from table 3, the surface area of ogbono shells  
 135 increased from 114cm<sup>2</sup> (raw ogbono shell) to 190.5cm<sup>2</sup> (esterified ogbono shell) after  
 136 modification with stearic acid thereby increasing the number of micropores within the surface  
 137 the biomass for oil sorption and further validates the effectiveness of biomass modification by  
 138 esterification and ogbono shells as a good sorbent for oil removal. Similar results on acetylated  
 139 ogbono shell (199.3cm<sup>2</sup>) has been reported by Alothman et al., (2011)

140 Table 3: Physical properties of the raw and modified ogbono shell

Adsorbents	Ash content (%)	Volatile matter (%)	Carbon content (%)	Surface area(m <sup>2</sup> /g)	pH
Raw ogbono shell	7.4	28.6	56.5	114	6.9
Carbonized ogbono shell	5.7	21.4	64.2	129.4	7.1
Esterified ogbono shell	5.6	19.3	69.4	190.5	7.2

141

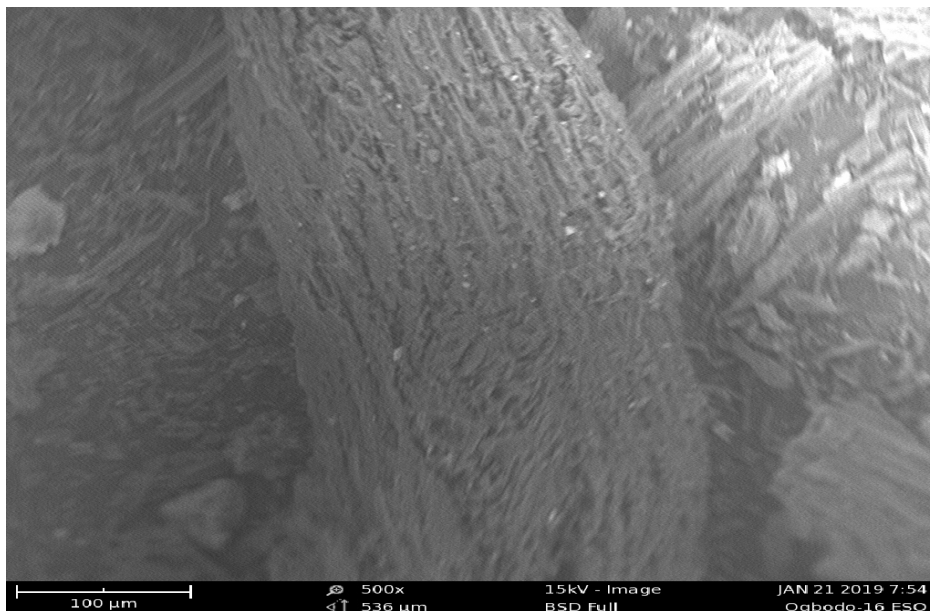
### 142 SEM Analysis Results

143 SEM Analysis is used to study the morphological compositions of the biomass before  
 144 modification and after modification. There were more pore spaces in the carbonized and  
 145 activated adsorbents than in the unmodified biomass. Availability of pore spaces favors  
 146 adsorption process since it is a surface reaction. The surface morphologies of the raw biomass  
 147 (Ogbono shells), and esterified biomass were presented as shown in fig 1 and 2. It was observed

148 from fig 1 that the samples were internally bonded together. It can be observed from the figures  
149 that a bulk of microstructure which in turn is composed of a homogeneously distributed network  
150 comprised of small filamentous and fistulous crystallites showing the presence of minerals. In  
151 the matrix, Luminous and non-luminous features can be seen. These features indicate the  
152 presence of minerals distributed in the organic matrix and as surface coverage. From fig 2, the  
153 surface is loosed and some features such as fissures, cleats, cracks and veins can be seen showing  
154 that the action of heat and acid did lots of harm to the surface and the surface is no longer as  
155 intact as shown in fig 1. Some minute fissures and cracks, however an evident. These changes in  
156 microstructures may not be unconnected to the removal of some minerals from the activated  
157 biomass thereby increasing the micro porous surface. The surface is bright and mostly  
158 protracted. That micrograph reveals that the activation has undergone properly. The porosity has  
159 been increased and provides strong evidence that significant amounts of organic elements are  
160 being removed thereby increasing the number of micro pores



161  
162 **Fig 1:** SEM image of un-carbonized ogbono shell @ 100µm  
163



164  
165 Fig 2: SEM image of esterified ogbono shell@ 100μm  
166

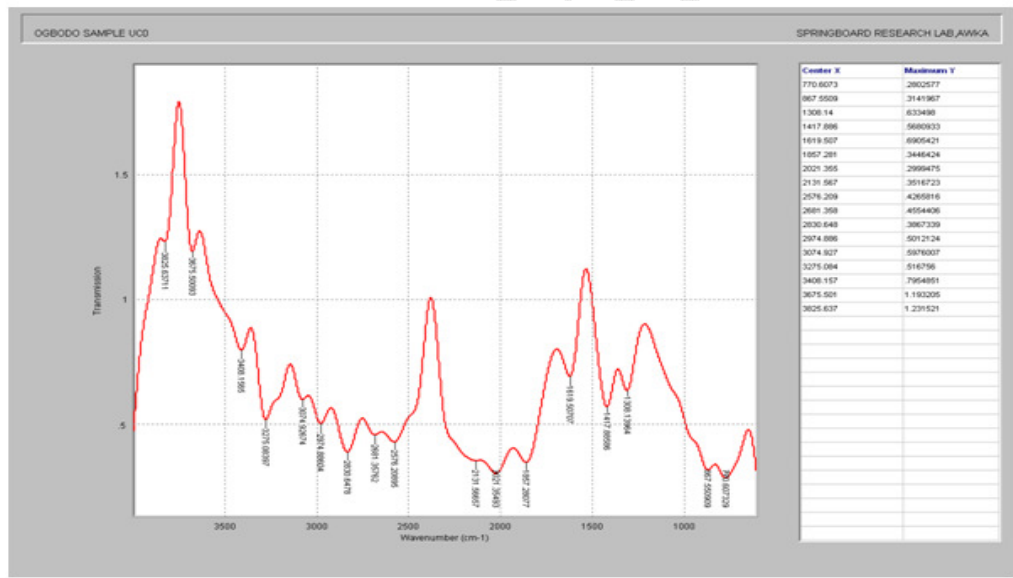
### 167 **Fourier Transform infrared (FTIR) of the modified and unmodified biomass**

168 Bands were assigned according to the published article (Starsinic et al., 1984; Supaluknari et al.,  
169 1998). Fourier transforms infrared spectra of the raw biomass, carbonized biomass, and esterified  
170 biomass are presented in Fig 3 to 5. The frequencies were assigned to the respective functional  
171 ground and interpreted. It was observed that the biomass sample (ogbono shell) have numerous  
172 functional groups and the major functional groups present are O-H, N-H, N-CH<sub>3</sub>, C=C-C, C-Cl,  
173 Si-O-Si. Petroxides bands stretches between 9650-1095cm<sup>-1</sup>, Aromatic phosphate P-O-C  
174 stretches between 1300-1390cm<sup>-1</sup>, Aromatic C-H in plane bend, Silicon ozy compounds Si-O-Si  
175 stretches between 1125-1295cm<sup>-1</sup>, C-Cl stretch, alkyne C-C bend lies between 700-900cm<sup>-1</sup>,  
176 hydroxyl group OH stretch was observed between 4000-3650cm<sup>-1</sup>, primary amine group NH  
177 stretches between 3200-3450cm<sup>-1</sup>, Aliphatic secondary amine NH stretches between 3150-  
178 3200cm<sup>-1</sup>, Normal polymetric stretch of hydroxyl group lies between 3050-3100cm<sup>-1</sup>,  
179 Methylamino acids N-CH, C-H stretches between 2550-2950cm<sup>-1</sup>, Cyanide ion, thiocyanide ion  
180 stretches between 1990-2000cm<sup>-1</sup>, Isocyanate N=C=O stretches between 2290-2550cm<sup>-1</sup>,  
181 Isothiocyanate -CNS bond stretches between 1600-1795cm<sup>-1</sup>, Conjugated keton, open chain acids  
182 anhydrides stretches between 1600-1750cm<sup>-1</sup>, the bending of the hydroxyl group was further  
183 observed at the stretch between 1450-1595cm<sup>-1</sup>. Fig 3 showed that the entire spectrum had more  
184 or less similar broad characteristic absorption bands. All the absorption bands were unresolved



185 indicating that the material constituents had either large particle size or a contained polymeric  
 186 unit which shows that the volatile matter is still intact. Esterification of the carbonized biomass  
 187 has better modification with removal of volatile matter thereby creating more pores for oil  
 188 adsorption as shown in fig 5 indicating that the picks are more resolved than the picks as shown  
 189 in Fig 3, this further proved that esterification is effective in removing volatile matter and  
 190 increasing micro pores on the surface of the adsorbents. The change in absorption and frequency  
 191 in the spectrum peaks shows how the several treatment conditions affect the structure of the  
 192 biomass .The functional groups indicate that the biomasses are organic compound which are  
 193 hydrophobic and olephilic. This could be the reasons while they were able to remove the oil from  
 194 water surface. Upon comparing the spectrum; it was observed that all the samples showed a  
 195 remarkable absorption near  $1440\text{cm}^{-1}$ . This indicated the strong presence of ethylene and methyl  
 196 groups in the samples. The bands at  $1541\text{cm}^{-1}$  and  $1442\text{cm}^{-1}$  is normally present in organic  
 197 substance (biomass) with more Lignin content. The band was shifted from strong absorption to  
 198 medium intensity in the spectra of stable product. This reveals the effectiveness of modification  
 199 of biomass using esterification.

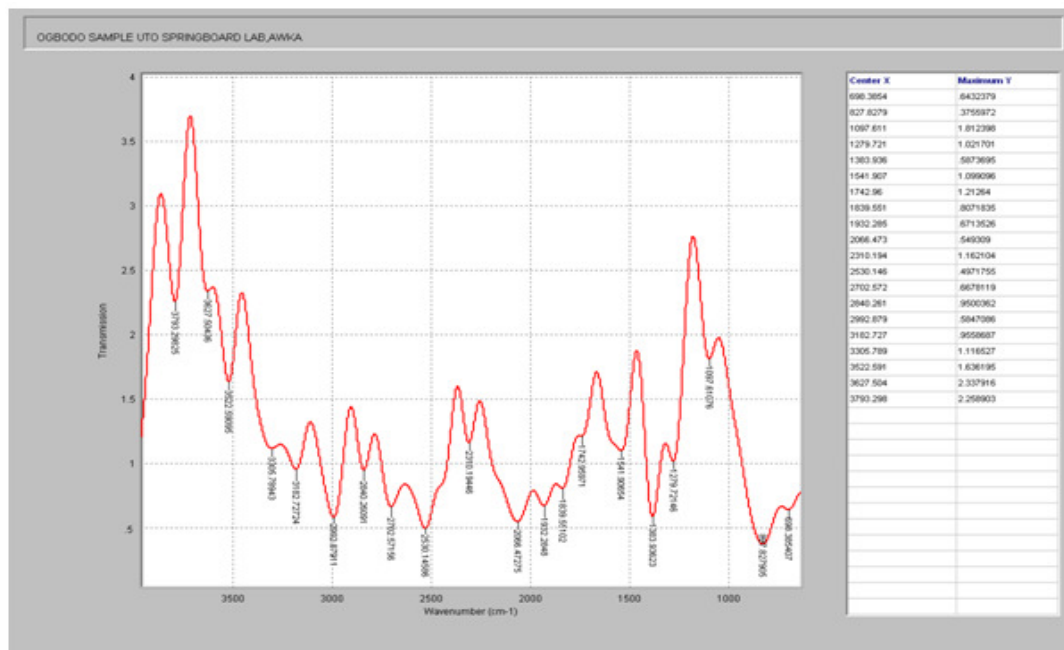
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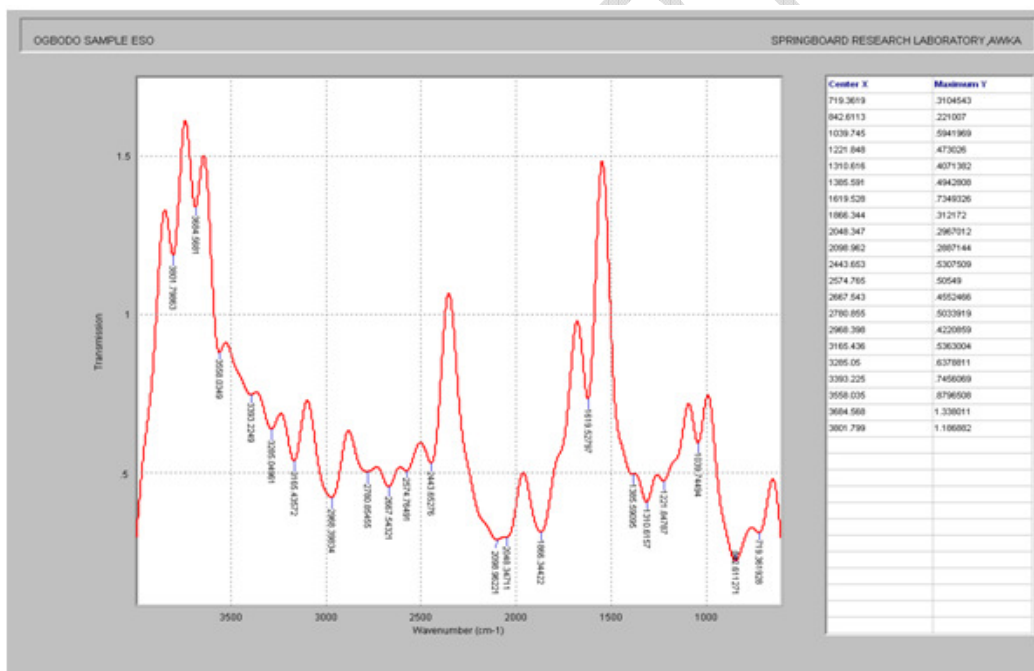
202 Fig 3: FTIR spectra for uncarbonized ogbono shell

203



204

205 Fig 4: FTIR spectra for carbonized ogbono shell



206

207 Fig 5: FTIR spectra for esterified ogbono shell

208 **Statistical analysis of the sorption process using RSM**

209 The process was optimized using Box Benkhen Design. This was done to determine the best  
 210 conditions for optimum sorption of the crude oil. In this work, a set of 27 experiments was

211 performed with the adsorbent (esterified ogbono shell) using a statistical package Minitab  
 212 software version 17.0. During analysis, it was discovered that the major response in which the  
 213 main parameters or factors were significant at 0.05 was percentage removed (%R). The  
 214 optimization analysis was therefore based on percentage removal as the major response. The  
 215 experiments were performed in random to avoid systematic error. The design matrix and output  
 216 responses for the sorption of crude oil were given in Table 2. The responses obtained from  
 217 various runs are significantly exceptional which implies that each of the factors have substantial  
 218 effect on the response.

219 **Analysis of variance (ANOVA) for the sorption of oil layer onto fatty acid grafted ogbono**  
 220 **shell**

221 The response values in Table 2 were analyzed using statistical package Minitab software  
 222 (Minitab version 17.0). The F-value tests were performed using the ANOVA to calculate the  
 223 significance of each type of model. Based on the results of F-value, the highest order model with  
 224 significant terms which shows the most accurate relationship between parameters was be chosen.  
 225 Besides evaluating the significance, the adequacy of the models was evaluated by applying the  
 226 lack-of-fit test. This test was used in the numerator in an F-test of the null hypothesis and  
 227 indicates that a proposed model fits well or not. The test for lack-of-fit compares the variation  
 228 around the model with pure variation within replicated observations. This test measured the  
 229 adequacy of the different models based on response surface analysis (Chauhan and Gupta, 2004)).  
 230 The sum of square, the degree of freedom, the mean square, the F-values were shown in Table 4.

231 Table 4: Analysis of Variance (ANOVA) for the sorption of oil onto esterified ogbono shell  
 232

Source	DF	Seq SS	Contribution	Adj SS	Adj MS	F-Value	P-Value
Model	6	1794.50	93.98%	1794.50	299.084	52.08	0.000
Linear	3	630.20	33.01%	630.20	210.065	36.58	0.000
X <sub>1</sub>	1	515.09	26.98%	515.09	515.092	89.70	0.000
X <sub>2</sub>	1	100.34	5.26%	100.34	100.341	17.47	0.000
X <sub>4</sub>	1	14.76	0.77%	14.76	14.763	2.57	0.025
X <sub>4</sub> <sup>2</sup>	1	347.35	18.19%	347.35	347.346	60.49	0.000
X <sub>1</sub> X <sub>2</sub>	1	373.65	19.57%	373.65	373.649	65.07	0.000
X <sub>2</sub> X <sub>4</sub>	1	443.31	23.22%	443.31	443.313	77.20	0.000

Error	20	114.85	6.02%	114.85	5.742		
Lack-of-Fit	18	94.17	4.93%	94.17	5.232	0.51	0.832
Pure Error	2	20.67	1.08%	20.67	10.337		
Total	26	1909.35	100.00%				

233	R-sq	R-sq(adj)	PRESS	R-sq(pred)
234	93.98%	92.18%	209.018	91.05%
235				

236 Multiple regression analysis was employed as a tool in this work to for the assessment of the  
 237 effect of independent variables (Time, temperature, dosage and pH) on the dependent variables  
 238 (%Sorption). % Sorption by the activated biomass (esterified ogbono shell) was analyzed using  
 239 multiple regression method to fit second order polynomial equations. The second order  
 240 polynomial equations developed after analysis of percentage sorption as a function of the actual  
 241 values of Time ( $X_1$ ), temperature ( $X_2$ ), dosage ( $X_3$ ) and pH ( $X_4$ ) are as follows;

$$242 \text{ (%Sorption)_{esterified ogbono shell} = } 88.36 - 1.0353 X_1 - 1.1615 X_2 + 0.77 X_4 + 0.01289 X_1 X_2 \\ 243 + 0.08773 X_2 X_4 - 0.4511 X_4^2 \quad (4)$$

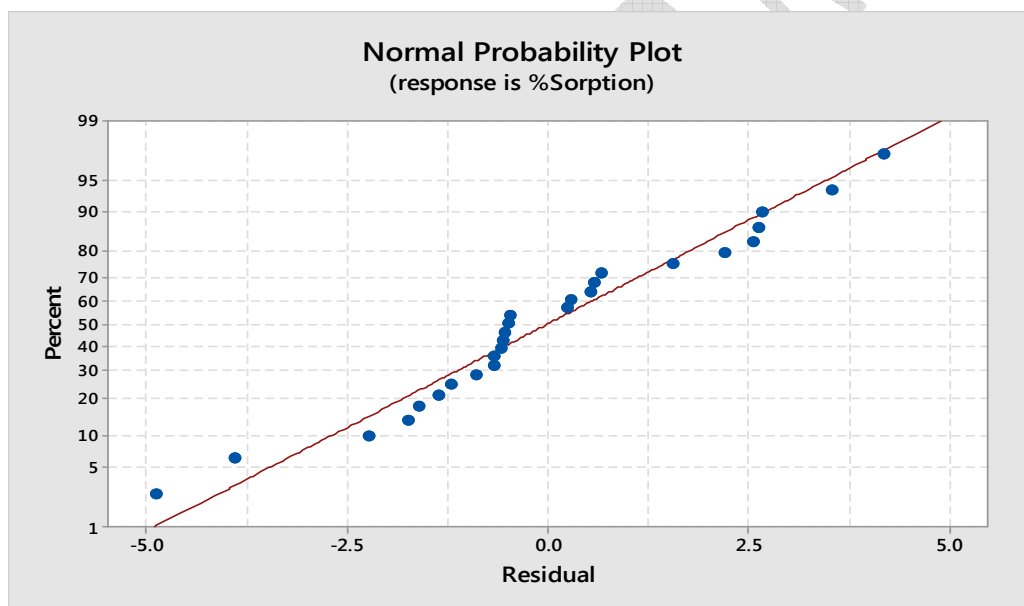
244  
 245 Regression coefficients of the intercept, linear, quadratic and interaction terms of each model  
 246 were presents in Table 4. The coefficient of determination ( $R^2$ ) obtained for the percentage  
 247 sorption of oil by esterified ogbono shell was 93.98%. These result shows that more that 93% of  
 248 the overall system variables can be explained by the quadratic models of equation 4. Higher  
 249 values of F-ratio and lower p-values indicated higher significance of the model or model terms.  
 250 The models significance was tested at  $p < 0.05$ .

251 It was observed that the model p-value was 0.000. This indicates that the model is very  
 252 significant and could be very efficient in predicting the system response (sorption of oil by  
 253 activated biomass). The F-values was also observed to be 52.08 for acetylated ogbono shell. This  
 254 value was found to be very high and as such, show that the model is highly significant above  
 255 93% confidence level. Table 4 shows that the linear terms of time ( $X_1$ ), temperature ( $X_2$ ) and pH  
 256 ( $X_4$ ) as well as interactive terms of time and temperature ( $X_1 X_2$ ), temperature and pH ( $X_2 X_4$ )  
 257 together with quadratic term of pH ( $X_4^2$ ) were all significant with p-values ( $p < 0.05$ ). However,  
 258 the adjusted coefficient of regression (Adj  $R^2$ ) and the predicted coefficient of regression (Pred  
 259  $R^2$ ) were found to be, 92.18% and 91.05%. These results are indication of the model significance

260 and also indicate that the quadratic model provided an excellent explanation for the relationship  
261 between the independent variables and the corresponding response.

262 The models adequacy was additionally checked from the normal residual plots as shown in Fig  
263 6. It can be seen from the figure that the residual followed the normal distribution and the assumption  
264 of normality is somewhat valid. The data were also analyzed to check the correlation between the  
265 experimental and predicted sorption (%R). The experimental values were the measured response data  
266 for the runs designed by the Box Benkhen model on the platform of Minitab software version 17.0,  
267 while the predicted values were obtained by calculation from equation 4. Also, the points were  
268 closely distributed to the striaght line of the plot ( $R^2 = 93.98\%$ ). This confirms the good  
269 relationship between the experimental values and the predicted values as shown in Table 2.  
270 Some small scatter like an “S” shape is always expected which shows a normal distribution of  
271 experimental data points within the straight line. These plots equally confirmed that the selected  
272 model was adequate in predicting the response variables.

273



274

275 Fig 6: Normal plot of residual for the sorption of oil onto esterified ogbono shell

276 **The Three Dimensional (3-D) response surface plots for crude oil adsorption onto fatty acid**  
277 **grafted ogbono shell.**

278 The 3-D response surface and contour plots are presented in Fig 7 and 8. The 3-D response  
279 surface and contour plots are graphical representation of the interactive effects of any two

280 variable factors. Response surface plots as a function of two factors at a time, maintaining all  
281 other factors at fixed levels are more helpful in understanding both the main and the interaction  
282 effects of these two factors. These plots can be easily obtained by calculating from the model, the  
283 values taken by one factor where the second varies with constraint of a given Y value. The  
284 response surface curves were plotted to understand the interaction of the variables and to  
285 determine the optimum level of each variable for maximum responses.

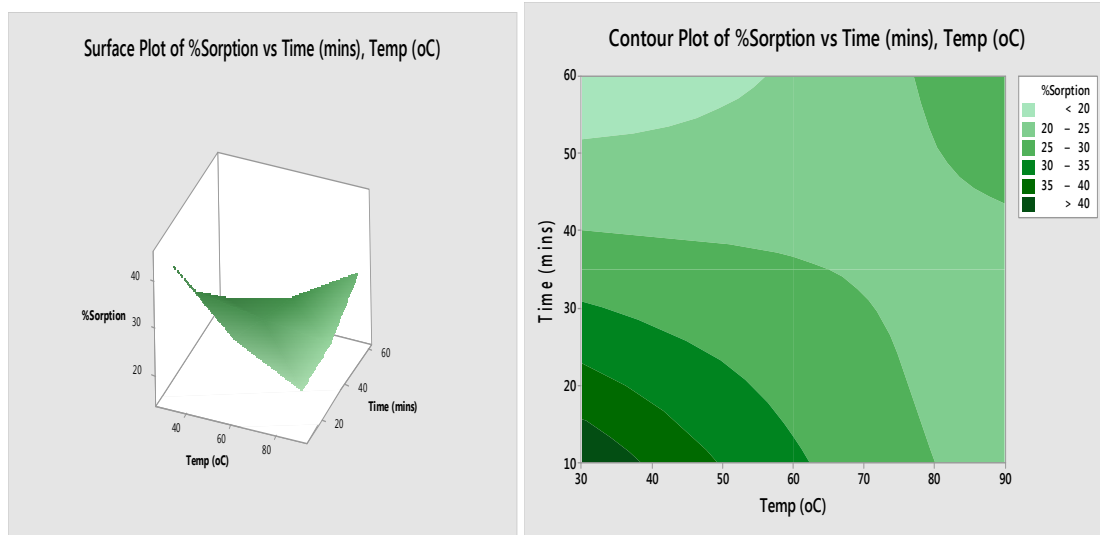
286 The nature of the response surface curves shows the interaction between the variables. The  
287 elliptical shape of the curve indicates good interaction of the two variables. From figures, it was  
288 observed that the elliptical nature of the contour in graphs depicts the interactions of all the  
289 variables. There was a relative significant interaction between every two variables, and there was  
290 a maximum predicted yield as indicated by the surface confined in the smallest ellipse in the  
291 contour diagrams.

292

### 293 **Temperature – Time interaction effect**

294 The temperature –time interaction effect was plotted against oil sorption and presented as shown  
295 in fig 7. Keeping every other factor constant, it was observed that the contour lines for the effect  
296 of temperature and time interactions were somewhat curve and circle indicating a good  
297 interaction. The contour lines showed that the interactions are significant. The significant level  
298 was proven by the p-values as shown in Table 4 which indicates that the p-values were less than  
299 0.05. It can be concluded that increase in temperature and time, increases the rate of oil sorption  
300 by the activated biomass. The interaction of temperature and time ( $X_1X_2$ ) was included in the  
301 model equation 4 for improvement of the model performance since the interactions are  
302 significant.

303



304  
305

306 Fig 7 : Response surface and contour plots for the effect of time and temperature on sorption of  
307 oil by fatty acid grafted ogbono shell.

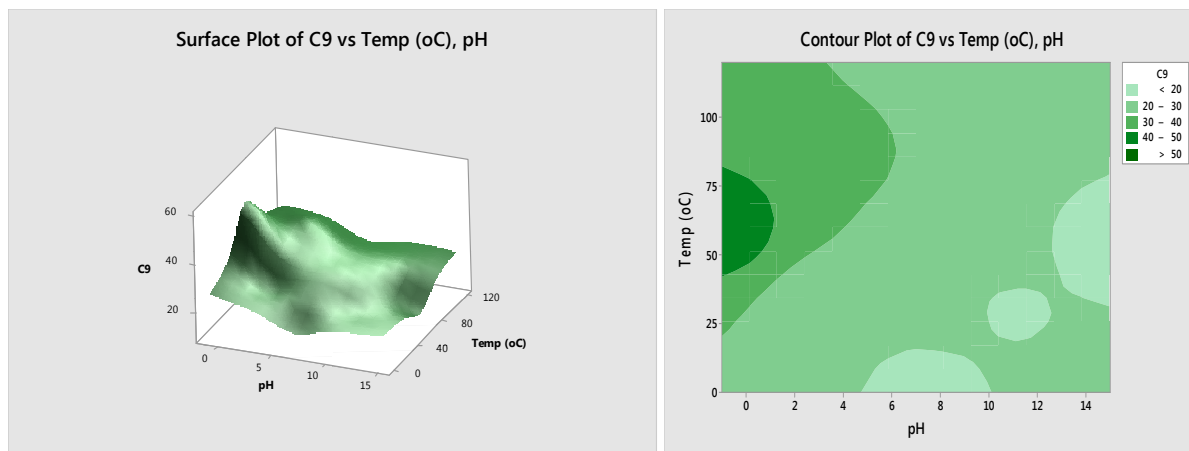
308

### 309 **pH- Temperaure interaction effect**

310

311 The pH- temperature effect ( $X_2X_4$ ) was included in equation 4 to improve the model  
312 performance. Fig 8 shows the response surface plot and contour plot for the effect of pH-  
313 temperature interaction on the percentage sorption of oil by the activated biomass. From the  
314 figure, the shape of the contour is curve showing a good interaction. The 3D plots also showed  
315 that almost equal percentage sorption could be obtained at low temperature, low pH; low  
316 temperature, high pH, high temperature, low pH; and high temperature, high pH. The height of  
317 the 3D seems to be the same at the four edges of the curve. The p-value of the curve is less than  
318 0.05 which indicates that the interaction is statistically significant.

319



320  
 321 Fig 8: Response surface and contour plots for the effect of pH and temperature on soption of oil  
 322 by esterified ogbono shell  
 323

324 **The numerical optimum conditions**

325 The developed model as shown in equation 4 for the process parameters was optimized using  
 326 response optimizer facility that is available on Minitab software version 17.0 which provided  
 327 several numerical optimum solutions. The optimization is also interactive and allows for the  
 328 compromise among the various independent variables and responses (Yuksel et al., 2006; Yi et  
 329 al., 2010). The optimum solutions are given in Table 5. the optimum time, temperature, dosage,  
 330 pH and percentage removal were; time of 10mins, temperature of 60°C, dosage of 1.4g, pH of 3  
 331 at the theoretical percentage removal of 78.77%. The theoretical percentage removal was  
 332 verified by carrying out adsorption process using the optimum parameters. The result of the  
 333 verified experiment was recorded as the actual percentage removal. The actual percentage  
 334 removal was in close agreement with the theoretical value as shown in table 5.

335 Table 5: The theoretical optimum solution using esterified ogbono shell

No.	Time (min)	Temp (°C)	Dosage (g)	Predicted (%R)	Actual (%R)	
1	10.0	60	1.4	78.77	76.40	Selected

336  
 337  
 338 **Conclusion**  
 339 Comparative study of data in this research revealed that carbonized ogbono shell modified by  
 340 esterification process using steric acid can be used as an eco-friendly adsorbent for the maximum



341 removal oil layer from oil polluted water surface. FTIR analysis of activated and uncarbonized  
342 biomass (ogbono shell) shows that they consist mainly of organic compounds such as hydroxyl  
343 group, amino group, amine, isocyanate, conjugated ketons, silicon, peroxide. Surface  
344 morphological analysis of raw and esterified ogbono shell using Scan electron microscope  
345 (SEM) revealed that activation of the biomass increased the surface area significantly. Statistical  
346 analysis of the sorption of oil onto activated biomass such as (esterified ogbono shell) showed  
347 that the process can be modeled by central composite design with all the four variables affecting  
348 the process such as .time, temperature, dosage and pH been statistically significant

349

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